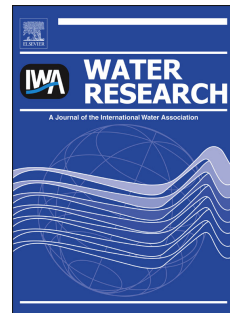


Accepted Manuscript

Title: The impact of differing cell and algogenic organic matter (AOM) characteristics on the coagulation and flotation of algae

Authors: Rita K. Henderson, Simon A. Parsons, Bruce Jefferson



PII: S0043-1354(10)00256-3

DOI: [10.1016/j.watres.2010.04.016](https://doi.org/10.1016/j.watres.2010.04.016)

Reference: WR 7968

To appear in: *Water Research*

Received Date: 13 January 2010

Revised Date: 16 April 2010

Accepted Date: 16 April 2010

Please cite this article as: Henderson, R.K., Parsons, S.A., Jefferson, B. The impact of differing cell and algogenic organic matter (AOM) characteristics on the coagulation and flotation of algae, *Water Research* (2010), doi: [10.1016/j.watres.2010.04.016](https://doi.org/10.1016/j.watres.2010.04.016)

This is a PDF file of an unedited manuscript that has been accepted for publication. As a service to our customers we are providing this early version of the manuscript. The manuscript will undergo copyediting, typesetting, and review of the resulting proof before it is published in its final form. Please note that during the production process errors may be discovered which could affect the content, and all legal disclaimers that apply to the journal pertain.

1 The impact of differing cell and algogenic organic matter (AOM)
2 characteristics on the coagulation and flotation of algae

3

4 RITA K. HENDERSON[#], SIMON A. PARSONS AND BRUCE JEFFERSON*

5

6 *Centre for Water Science, Cranfield University, Cranfield, BEDFORDSHIRE, MK43*
7 *0AL, UK*

8 # Current address: UNSW Water Research Centre, University of New South Wales,
9 NSW 2052, Australia

10 *Corresponding author: b.jefferson@cranfield.ac.uk

11 Tel: +44 (0) 1234 750111; Fax: +44 (0) 1234 751671

12

13 **Abstract:**

14 The aim of this study was to compare the coagulation and flotation of different algae
15 species with varying morphology and algogenic organic matter (AOM) composition
16 in order to link physical and chemical algae characteristics to treatment. *Microcystis*
17 *aeruginosa* (cyanobacteria), *Chlorella vulgaris* (green algae), *Asterionella formosa*
18 and *Melosira* sp. (diatoms) were treated by coagulation with aluminium sulphate and
19 flotation. The AOM was extracted and treated separately. Analyses included cell
20 counts, dissolved organic carbon, aluminium residual and zeta potential. Removal
21 efficiencies in the range 94-99 % were obtained for each species. Cells, AOM and
22 aluminium were concurrently removed at a coagulant dose that was related on a log-
23 log basis to both cell surface area and total charge density, although the relationship
24 was much stronger for the latter. This was attributed to a significant proportion of the
25 coagulant demand being generated by the AOM. The implications of such findings

26 are that relatively simple charge measurements can be used to understand and control
27 coagulation and flotation of algae.

28

29 **Introduction**

30

31 Algae are ubiquitous in rivers and reservoirs that supply drinking water treatment
32 works. On a seasonal basis, algae population densities can soar, challenging the
33 removal efficiency of treatment processes. A commonly employed treatment chain for
34 algae removal is coagulation-flocculation-dissolved air flotation (DAF). During DAF
35 treatment, negatively charged, microscopic bubbles collide and attach to influent
36 particles, floating them to the surface where they are removed. Successful flotation is
37 reliant upon influent particles having both a minimum particle diameter of
38 approximately 10-30 μm (Edzwald, 1995), and a surface charge that approaches
39 neutral (Han et al., 2001), equating to a zeta potential of approximately -10 mV to +5
40 mV (Henderson et al., 2008d), to ensure effective particle-bubble collision and
41 attachment efficiencies respectively. Algae are negatively charged and many common
42 species are less than 10 μm in diameter therefore coagulation and flocculation
43 processes are included to adjust the size and charge of the algae cells accordingly. If
44 coagulation is unsuccessful, poor flotation can occur which results in high coagulant
45 and cell residuals causing downstream filter blockage or breach (Henderson et al.,
46 2008a, Henderson et al., 2008b). Residual algal matter can form disinfection by-
47 products (DBP) such as trihalomethanes (THM) (Chen et al., 2008, Nguyen et al.,
48 2005) or be responsible for offensive taste and odour compounds or toxic metabolites
49 (Haider et al., 2003, Rosen et al., 1992).

50 Coagulation of algae cells can be difficult as a result of their widely variable
51 physical and chemical characteristics (Henderson et al., 2008b), including complex
52 cell morphologies, such as spinal appendages preventing close contact of cells
53 (Bernhardt and Clasen, 1991); cell motility, enabling liberation from flocs (Pieterse
54 and Clout, 1997); variable surface charge (Henderson et al., 2008d); or algogenic
55 organic matter (AOM) sterically interfering to prevent agglomeration, increasing the
56 negative charge at the cell surface and complexing with metal coagulants thus raising
57 residual coagulant concentration (Bernhardt et al., 1985, Pivokonsky et al., 2006,
58 Takaara et al., 2004). These characteristics generally act to increase coagulant
59 demand and it has been suggested that consequently coagulant cannot be added on a
60 stoichiometric basis (Bernhardt et al., 1985), as is usual for inert, inorganic particles
61 (Stumm and O'Melia, 1968). Earlier studies suggested that only microscopic,
62 spherical cells can be coagulated according to charge neutralisation mechanisms
63 (Bernhardt and Clasen, 1994, Tilton et al., 1972) thus allowing optimum coagulant
64 dosage to be estimated stoichiometrically. However, these conclusions resulted from
65 studies investigating coagulation followed by direct filtration and may not apply for
66 flotation processes. While numerous studies on the flotation of algae have been
67 conducted (Edzwald, 1993, Kempeneers et al., 2001, Teixeira and Rosa, 2006), no
68 studies have investigated the link between coagulation-flotation and algal
69 characteristics. Specifically, the impact of variable morphology and AOM
70 composition on coagulation and removal by flotation requires investigation and this
71 will be the focus of the current paper.

72 The authors recently undertook a study examining the AOM characteristics of four
73 algae species –*Chlorella vulgaris* (micro, spherical, green algae), *Microcystis*
74 *aeruginosa* (micro, spherical cyanobacteria), *Asterionella formosa* (large, elongated,

75 colonial diatom), and *Melosira* sp. (large, filamentous diatom) (Henderson et al.,
76 2008c) (Table 1). The major differences in AOM characteristics were associated with
77 charge density, hydrophobicity, protein content and molecular weight (MW). AOM
78 from *C. vulgaris* had a charge density of 3.2 meq g⁻¹ and a hydrophobicity of 11 %
79 whereas that of *M. aeruginosa* had a charge density of 0.1 meq g⁻¹ and a
80 hydrophobicity of 30 %. Much less protein was present in AOM extracted from the
81 diatoms - *A. formosa* and *Melosira* sp., compared with *C. vulgaris* and *M. aeruginosa*.
82 Additionally, *C. vulgaris* and *M. aeruginosa* had larger MW AOM in comparison to
83 *A. formosa* and *Melosira* sp., where 45 % of *M. aeruginosa* AOM was greater than
84 500 kDa in comparison to less than 10 % of *C. vulgaris* AOM (Henderson et al.,
85 2008c). It is anticipated that the differences may impact considerably on coagulant
86 dose for optimum removal. Hence, the major objective of this study was to treat the
87 aforementioned algal cultures using coagulation-flocculation-DAF and link the
88 coagulation conditions required for treating each species by flotation to algal physical
89 and chemical character.

90 *Insert Table 1*

91

92 **Materials and Methods**

93

94 **Algae Cultivation.** The following freshwater algae cultures were obtained from the
95 Culture Collection of Algae and Protozoa (CCAP), (Oban, Scotland): *Chlorella*
96 *vulgaris* (211/11B – Delft, Holland); *Microcystis aeruginosa* (1450/3 – Esthwaite
97 Water, Cumbria, England); *Asterionella formosa* (1005/9 – Esthwaite Water,
98 Cumbria, England), while *Melosira* sp. (JA386 – Redesmere, Cheshire, England) was
99 obtained from Sciento, Manchester, UK. Growth conditions have previously been

100 described (Henderson et al., 2008c). Algae were harvested for experiments in the
101 early stationary phase.

102

103 **AOM Extraction.** AOM was extracted from all bulk algae suspensions with the
104 exception of *Melosira* sp. by centrifuging at 10,000 G for 15 minutes and
105 subsequently filtering the supernatant through a 0.7 µm filter (Whatman GF/F glass
106 microfibre). AOM therefore comprises both extracellular organic matter (EOM), any
107 intracellular organic matter (IOM) that may have been present, and also loosely bound
108 organic matter, which may be dislodged via centrifugation (Henderson et al., 2008c)

109

110 **Algae Cell Characterisation.** The algae systems were assessed using the following
111 methods:

112 a) Cell concentration – a light microscope was used to manually count cells with a
113 haemocytometer and Sedgewick Rafter cells as appropriate. Samples were left to
114 settle onto the grids for 15 minutes. At least 100 cells were counted in triplicate.

115 b) Cell surface area – images of cells were obtained microscopically and sized using
116 a scale generated using a graticule. The dimensions were used to produce surface
117 areas using basic geometric shapes as follows: *C. vulgaris* and *M. aeruginosa*
118 were sized using a spherical surface area = $4\pi r^2$; *A. formosa* and *Melosira* sp. were
119 sized using a cylindrical surface area = $2\pi r^2 + 2\pi rh$. In each case the dimensions
120 of 100 cells were measured.

121 c) Charge density – The back titration method utilised was adapted from an
122 established method (Kam and Gregory, 2001). The specific procedure was that
123 utilised for determining AOM charge density was previously reported (Henderson
124 et al., 2008c). Three different volumes of algae were analysed.

125 d) Zeta potential – A Malvern Zetasizer 2000HSA (Malvern, UK) was utilised to
126 determine the zeta potential of the system.

127

128 **Coagulation and Dissolved Air Flotation.** Stock algae suspensions were diluted
129 prior to treatment to a concentration more often observed in supply reservoirs using
130 deionised water to which 0.5 mM NaHCO₃ and 1.8 mM NaCl had been added. See
131 Table 2 for initial algal concentrations. Bench scale coagulation and flotation was
132 undertaken using an EC Engineering Dissolved Air Flotation Batch Tester, Model
133 DBT6 (Alberta, Canada). Aluminium sulphate coagulant was added to 1 litre of algae
134 suspension at the beginning of a 2 minute rapid mix (200 rpm), during which pH was
135 adjusted to either pH 5 or 7 using 0.1 M NaOH or 0.1 M HCl as required.
136 Coagulation and flotation experiments were undertaken at pH 7 for all algae species
137 and additionally at pH 5 for *M. aeruginosa* and *C. vulgaris*. It has previously been
138 observed that algae may not start agglomerating until more than 7 minutes of slow
139 mixing has passed (Henderson et al., 2006), attributed to a lag time in charge
140 neutralisation (Clasen et al., 2000). For this reason flocculation time was 15 minutes
141 of slow mixing (30 rpm) rather than 5 minutes which is usually more normal for
142 flotation processes. After flocculation, the paddles were gently removed and air
143 saturated deionised water with 0.5 mM NaHCO₃ and 1.8 mM NaCl was supplied at a
144 pressure of 450 kPa and recycle ratio of 12 %. The algae-bubble agglomerates were
145 allowed to float for 10 minutes.

146 Samples of the clarified water were obtained from sampling ports located 5 cm
147 from the vessel base for analyses by cell count and zeta potential as previously
148 described and DOC using a Shimadzu TOC-5000A analyser. All analyses were
149 performed in triplicate.

150 The same coagulation-DAF experiment was also undertaken for AOM
151 extracted from *C. vulgaris*, *M. aeruginosa* and *A. formosa* at pH 7. Samples were
152 adjusted to approximately 5 mg L⁻¹ by dilution using deionised water with 0.5 mM
153 NaHCO₃ and 1.8 mM NaCl. At the early stationary phase, cell concentrations for *C.*
154 *vulgaris*, *M. aeruginosa* and *A. formosa* were 1.2 x 10⁷ cells mL⁻¹, 1.5 x 10⁷ cells mL⁻¹
155 and 2.9 x 10⁵ cells mL⁻¹ respectively., thus requiring the extraction of approximately
156 140 mL, 350 mL and 900 mL respectively of algae per jar test to provide sufficient
157 AOM. Subsequent analyses included residual aluminium by atomic absorption
158 spectroscopy using a Perkin Elmer AAnalyst 800 (Perkin Elmer, Beaconsfield, UK),
159 DOC and zeta potential.

160

161 **Results and Discussion**

162

163 **Algae System Characterisation**

164

165 *M. aeruginosa* and *C. vulgaris* cells are microscopic spherical cells and therefore had
166 far greater initial cell concentrations and smaller individual cell surface areas when
167 compared with the much larger diatoms of *A. formosa* and *Melosira* sp. (Table 2).
168 Charge equivalents, presented on a per cell basis, were in the range 0-1.88 peq cell⁻¹
169 where *M. aeruginosa* had the smallest charge density and *Melosira* sp. the largest.
170 The charge density of each species increased with increasing pH. This is attributable
171 to dissociation of carboxylic acid groups, similar to that observed for natural organic
172 matter (NOM) (Kam and Gregory, 2001). AOM concentration for the cell
173 concentrations examined in this study were in the range 0.6-1.5 mg L⁻¹ as C. By
174 comparison of the charge density of AOM alone (Table 1) and the whole system of

175 cells and AOM, an estimate of the contribution of charge by AOM was calculated.
176 AOM was found to contribute 84%, 5% and 30% of the charge of the system for *C.*
177 *vulgaris*, *M. aeruginosa* and *A. formosa* respectively while for *Melosira* sp. the AOM
178 had negligible charge density (Table 2).

179 *Insert Table 2*

180

181 **Algae-Coagulant Interactions**

182

183 A log linear relationship between the ratio of the coagulant dose (as aluminium) to
184 cell charge equivalence (coagulant:charge ratio) and the zeta potential was observed
185 for all four algae systems coagulated at pH 7 (Figure 1). This relationship is relevant
186 as it quantifies the effectiveness of coagulant in neutralising the charge of the algal
187 system. Figure 1A depicts the relationship when coagulation the entire algal system,
188 including cells and associated AOM, while Figure 1B shows the relationship when
189 coagulating only AOM extracted by centrifuging and filtration. The gradients of the
190 log-linear relationships in Figure 1A were 22.8, 13.6, 9.5 and 11.0 mV meq⁻¹ for
191 *C. vulgaris*, *M. aeruginosa*, *A. formosa* and *Melosira* sp respectively, indicating that
192 the coagulant was significantly more effective at neutralising the charge of *C. vulgaris*
193 in comparison to the other three species. The coagulant:charge ratios required to
194 achieve neutralisation were 183, 456, 1290 and 2781 mg meq⁻¹ for *Melosira* sp., *C.*
195 *vulgaris*, *A. formosa* and *M. aeruginosa* respectively. These ratios are comparable
196 with the literature as one study determined that the spherical cyanobacteria,
197 *Synechocystis minuscular*, required a coagulant (Al):charge ratio of 1400 mg meq⁻¹ at
198 pH 6 for complete neutralisation (Bernhardt and Clasen, 1994).

199 The resulting gradients for Figure 1B were 16.3, 20 and 11.5 mV meq mg⁻¹ for
200 *C. vulgaris*, *M. aeruginosa* and *A. formosa* respectively and thus, while the gradient
201 obtained for *A. formosa* was very similar to that observed for the entire system, those
202 of *C. vulgaris* and *M. aeruginosa* were less than and greater than those obtained for
203 the entire system, respectively. The coagulant:charge ratio required to achieve
204 neutralisation for *C. vulgaris* was 263 mg meq⁻¹, as opposed to the much larger values
205 of 2426 and 6017 mg meq⁻¹ for *A. formosa* and *M. aeruginosa* respectively. The
206 coagulant:charge ratio was therefore 1.7 times less than that required for
207 neutralisation of the entire *C. vulgaris* system while that of *A. formosa* and *M.*
208 *aeruginosa* was 1.9 and 2.2 times greater.

209 *Insert Figure 1*
210
211

212
213 In general, differences observed in zeta potential vs coagulant dose curves are
214 explained in terms of varying pH, charge density or complexation of coagulant.
215 However, each experiment was conducted at the same pH and the coagulant dose was
216 normalised against the charge density of the algae or AOM. Hence, the different doses
217 required to achieve a neutral zeta potential and gradient reflect a difference in
218 coagulant interaction mechanism with the cells and AOM, particularly with respect to
219 complexation. It is known that at pH 7 the concentrations of dissolved cationic
220 hydrolysis products are relatively low and the system is dominated by the negatively
221 charged aluminate ion (Al(OH)₄⁻) and by amorphous Al(OH)₃ precipitate (Duan and
222 Gregory, 2003). This precipitate has an isoelectric point at pH 8 as a result of surface
223 ≡Al–OH⁺ groups and is thus positively charged at pH 7. Hence, surface complexation
224 is likely to occur between these cationic sites and dissociated –COOH groups which

225 are generally attributed to charge in an algae system (Bernhardt et al., 1985).
226 Adsorption of negatively charged AOM and cells to amorphous precipitates may also
227 occur such that a net decrease in negative charge results (Duan and Gregory, 2003).
228 A low gradient such as that exhibited by *A. formosa* indicates that this neutralisation
229 mechanism is relatively inefficient in comparison to larger gradients, such as that
230 exhibited by *C. vulgaris*.

231 Explanation for the differences in efficiency of neutralisation lies in the system
232 character and particularly that of the AOM as it will be closely associated with the
233 cells. For example, the *M. aeruginosa* system required approximately six times the
234 coagulant:charge ratio of *C. vulgaris* for complete neutralisation. This increased to 22
235 times in the case of the AOM. The AOM of *M. aeruginosa* has a very low charge but
236 a significant protein concentration of 0.64 mg protein mg⁻¹ DOC (Table 1) and, while
237 that of *C. vulgaris* is also significant at 0.40 mg protein mg⁻¹ DOC, previous studies
238 have demonstrated that only the cyanobacteria protein and not green algae proteins
239 have the appropriate characteristics for protein-coagulant complexation (Pivokonsky
240 et al., 2006; Takaara et al., 2004; Takaara et al, 2007). The fact that the gradient of
241 the AOM curve for *M. aeruginosa* was relatively steep but that charge neutralisation
242 was not instigated until a much larger coagulant:charge ratio had been achieved
243 suggests that initially aluminium coagulant was consumed by protein complexation
244 such that it was unavailable for charge neutralisation. In the case of *A. formosa*, the
245 relatively high coagulant:charge ratio that was required for neutralization relates to
246 both an increased point of onset of neutralization as well as a relatively low gradient.
247 To date, no studies have addressed the protein-coagulant complexation reactions from
248 AOM other than that extracted from *C. vulgaris* and *M. aeruginosa*. This represents
249 an area for future research, which would clarify the following proposed hypothesis.

250 The fact that the onset point of neutralization lies between the other two systems
251 infers a moderate influence of protein-coagulant complexation. However, comparison
252 of the protein:DOC ratio for the AOM from *A. formosa* reveals the lowest level of the
253 three at 0.2, suggesting that the protein complexing power of AOM from *A. formosa*
254 may be similar to that of *M. aeruginosa* and the difference may be just related to total
255 mass of available protein. In terms of the lower gradient, the size of the carbohydrates
256 appears important. In the case of *A. formosa* the carbohydrates were predominately
257 less than 1 kDa in size (81% of total) compared to 30% and 38% for the AOM from
258 *C. vulgaris* and *M. aeruginosa* respectively. These types of carbohydrates are known
259 to exhibit a low affinity for coagulant such that very large doses are required
260 (Bernhardt et al., 1985). The mechanism in this case is either a reduced complexation
261 process or direct adsorption onto precipitate. In either case, a shallower gradient can
262 be expected as each unit of coagulant has less impact.

263

264 **Removal Efficiencies of Cells, AOM and Aluminium**

265

266 ***Cell Removal***

267 There were four coagulation regions for *C. vulgaris* at pH 5 (Figure 2): Zone 1 – a
268 region of no removal at low doses; Zone 2 - an initial zone of removal at low dose that
269 coincided with a reduction in the magnitude of the zeta potential (ZP) to +3.8 mV;
270 Zone 3 - a restabilisation zone where ZP values were highly positive at +15 mV; and
271 Zone 4 – a secondary removal zone at high coagulant doses. Coagulant doses were
272 normalised to surface area which has previously been demonstrated to be a useful
273 preliminary indicator of coagulant dose (Henderson et al., 2008b). The coagulant
274 doses giving the maximum removal efficiency for Zone 2 and Zone 4 removal were

275 0.0195 g m⁻² (289 mg meq⁻¹) and 0.742 g m⁻² (11,027 mg meq⁻¹) respectively
276 achieving 97.7 % and 96.8 % removal respectively. This sequence of removal zones
277 is commonly observed for both organic and inorganic systems at pH 5, where Zone 2
278 removal is attributed to charge neutralisation mechanisms while Zone 4 is attributed
279 to sweep flocculation mechanisms (Duan and Gregory, 2003). In contrast, no
280 restabilisation zone was observed for *M. aeruginosa* at pH 5, even upon reaching
281 highly positive ZP values of +18.9 mV (Figure 2). Furthermore, in contrast to *C.*
282 *vulgaris*, a far lower dose of 0.0087 g m⁻² was required to obtain good removal
283 corresponding to a ZP of -4.2 mV. It is proposed that the absence of a restabilisation
284 zone is attributable to large MW proteins and carbohydrates acting as polymer aids
285 and overcoming repulsive electrostatic forces. This is supported by previous work
286 that showed that at pH 5 such polymers are only partially deprotonated (Bernhardt et
287 al., 1985). In contrast, it is suggested that AOM did not prevent restabilisation of *C.*
288 *vulgaris* systems at pH 5 as the AOM was smaller with ~5 % larger than 500 kDa
289 compared to ~45 % for *M. aeruginosa* (Henderson et al., 2008c) and therefore would
290 not be as efficient a polymer aid.

291 *Insert Figure 2*
292

293 At pH 7, no restabilisation zone was observed for any of the algae systems.
294 Optimum coagulant doses were 0.7 to 1.36 mg L⁻¹ as Al, which when normalised for
295 cell count were in the order 1.1 < 4.3 < 31.4 < 290 pg cell⁻¹ for *M. aeruginosa*, *C.*
296 *vulgaris*, *A. formosa* and *Melosira* sp. (Table 3). The value obtained for *M.*
297 *aeruginosa* is comparable with that obtained for the similar organism, *Synechocystis*
298 *minuscula*, which had a coagulant demand at pH 6 of 1 pg Al cell⁻¹ (Bernhardt and
299 Clasen, 1994). Doses per charge and surface area were also calculated as 383, 927,
300 508 and 154 mg Al meq⁻¹ and 0.078, 0.012, 0.085 and 0.053 pg μm⁻² for *C. vulgaris*,

301 *M. aeruginosa*, *A. formosa* and *Melosira* sp. respectively. Corresponding zeta
302 potentials at optimum removal were -14.5 ± 1.6 , -10 ± 2.2 , -13.5 ± 0.4 and 1.4 ± 0.3
303 mV for the same species. Optimum removal was similar for all species at between
304 94.8 and 99.7 % cells removed.

305 *Insert Table 3*

306
307 The dose required for *C. vulgaris* at pH 7 in terms of surface area was four times
308 higher than at pH 5 (Figure 2). This observation is a reflection of firstly the decrease
309 in charge density of the system, which was three times lower at pH 5. Secondly,
310 dissolved cationic hydrolysis species as opposed to amorphous hydroxide precipitates
311 dominate and these are more effective neutralisers. Interestingly, the corresponding
312 coagulant:charge ratio decreased by only 1.3 times, as it only reflected the difference
313 in alum speciation having already been normalised for charge density. In contrast, the
314 optimum coagulant demand of *M. aeruginosa* at pH 5 was $0.0087 \text{ pg } \mu\text{m}^{-2}$, only 1.4
315 times less than that required at pH 7. This is primarily a result of the change in alum
316 speciation as the charge density of these algae was much lower than that of *C.*
317 *vulgaris* and therefore less significant.

318
319

320 ***AOM Removal***

321 The coagulant dose required to achieve maximum removal of AOM was $0.8 < 1.2 <$
322 $1.5 \text{ mg Al mg}^{-1} \text{ DOC}$ for *C. vulgaris*, *M. aeruginosa* and *A. formosa* respectively
323 (Figure 3) at zeta potential values of 3.8 ± 0.8 , 1.0 ± 0.3 and -7.9 ± 0.7 mV for the
324 same species. Additionally, AOM was relatively treatable with removal efficiencies
325 of 71 %, 55 % and 46 % for *C. vulgaris*, *M. aeruginosa* and *A. formosa* respectively.
326 In general these removal efficiencies are greater than those observed in a previous

327 study where AOM was coagulated using ferric chloride and removed by
328 sedimentation to yield removal efficiencies of 18 %, 25 and 50 % at pH 5 for the
329 species *M. aeruginosa*, *Scenedesmus quadricauda*, *Dictyosphaerium pulchellum*
330 respectively (Widrig et al., 1996). The doses required to achieve maximum removal
331 efficiency are consistent with literature values for NOM which has a coagulant
332 demand of approximately 1 mg Al mg⁻¹ at neutral pH (Duan and Gregory, 2003). *M.*
333 *aeruginosa* required a larger dose than *C. vulgaris*, despite having a lower charge
334 density of 0.1 meq g⁻¹ compared with 3.2 meq g⁻¹ (Table 1), attributed to protein-
335 coagulant complexation increasing coagulant demand. The high coagulant demand of
336 *A. formosa* can be explained by the low MW AOM causing inefficient flocculation,
337 where cross linking of the small MW AOM-aluminium compounds is required to
338 build flocs. The high removal efficiency of *C. vulgaris* AOM is a result of the
339 material being both highly charged and of relatively large MW such that flocculation
340 is efficient.

341 *Insert Figure 3*

342 **Aluminium Residual**

343 Residual aluminium data revealed that high Al residuals of up to 65 % could be
344 anticipated for aluminium doses of less than 0.5 mg Al mg⁻¹ DOC at pH 7 (Figure 4).
345 The lowest aluminium residuals of 0.4 %, equating to a residual of 10-35 µg l⁻¹, were
346 achieved for doses of greater than 0.8 mg Al mg⁻¹ C (Figure 4), which is concurrent
347 with optimum AOM removal (Figure 3). This high initial residual and subsequent
348 lowering of aluminium at higher aluminium:DOC ratios has previously been observed
349 for humic acid systems, where a dose of 0.54 mg Al:mg C was required to ensure low
350 aluminium residuals (Jekel and Heinzmann, 1989). Similarly, a study examining the
351 coagulation of AOM originating from *Chlorella* with iron determined that residual

352 iron was always found in the filtrate for doses of $<0.2 \text{ mg Fe mg C}^{-1}$ but never at
353 doses of $1 \text{ mg Fe mg C}^{-1}$ (Bernhardt et al., 1985). This trend has been attributed to the
354 coordination of AOM to metal-hydroxide polymers at low concentrations thus
355 preventing the cross linking and clustering of Al-hydroxide polymers which
356 consequently only becomes possible at higher doses (Bernhardt et al., 1985, Jekel and
357 Heinzmann, 1989), when simultaneous removal of both AOM (Figure 3) and
358 aluminium (Figure 4) occurs. The fact that residual aluminium in the *M. aeruginosa*
359 systems was similar to those of *C. vulgaris* and *A. formosa* indicates that protein-Al
360 complexates did not remain dissolved in solution and were bound into flocs by the
361 aforementioned mechanisms.

362 While the treatability of cells, AOM and aluminium has been demonstrated,
363 their concurrent removal must also be considered. If cells were removed
364 preferentially, then high residual AOM and consequently high aluminium levels could
365 result. At the dosages required to achieve maximum removal of , the ratios of
366 coagulant:DOC were calculated to be 0.93, 1.4 and 1.7 mg as Al mg^{-1} DOC at pH 7
367 for *C. vulgaris*, *M. aeruginosa* and *A. formosa* respectively, such that each was greater
368 than the 0.8 mg mg^{-1} required for low residuals of both aluminium and AOM. Hence,
369 for the optimum coagulant doses, it is anticipated that removal of all three
370 components would result.

371 *Insert Figure 4*

372

373 **Relationships Between AOM Character and Removal**

374

375 The study demonstrated that, with appropriate application of coagulant, good removal
376 could be anticipated for all of three system components – cells, AOM and aluminium,

377 irrespective of algae species. The key difference between the systems was in the
378 coagulant dose required to achieve maximum removal. Analysis of the data presented
379 in this study, compared with that of another study (Bernhardt and Clasen, 1994)
380 reveals a log-log relationship between optimum dose and both cell surface area and
381 charge density (Figure 5). The relationship between coagulant dose and charge
382 density appears stronger than that of surface area, attributable to the fact that the
383 dissolved organic component is also taken into account in the former. This is most
384 important as the charge demand generated by some species is predominantly
385 associated with the AOM component. For instance, in the case of *C. vulgaris*, 84 %
386 of the charge is associated with the AOM. Other studies have reported a relationship
387 between the concentration of algae and coagulant dose and have attributed this to
388 increases in surface area and thus charge density (Stumm and O'Melia, 1968, Tilton et
389 al., 1972); however, these early studies were concerned with only one type of
390 microscopic, spherical algae. Extending the analysis across multiple species then
391 reveals the importance of understanding the impact of charge density in determining
392 the optimum dose (Figure 5). Detailed analysis of how the coagulant interacts with
393 AOM to reduce the charge reveals a number of different actions which describe the
394 zeta profiles away from the optimum point. The work presented here suggests the two
395 important characteristics of the associated AOM are the complexing strength of the
396 protein components and the size of the carbohydrates as they appear to influence the
397 onset point of neutralization and the rate of neutralization respectively. Together these
398 describe the how the zeta potential of the system changes with coagulant addition and
399 provides a route to determining the sensitivity of the system to changes in dose.
400 Further work is required to confirm such suggestions by detailed analysis of the
401 protein complexation relationships as previously reported for *C. vulgaris* and *M.*

402 *aeruginosa* (Takaara et al., 2004). However, if confirmed, these two components
403 provide potential diagnostic signals with which to track and predict changing
404 coagulation requirements for algal systems.

405 The findings outlined here indicate a similar relationship to that observed for
406 NOM, where coagulant dose was closely related to the charged component of the
407 water (Sharp et al., 2006). The implications of such findings are that relatively simple
408 charge measurement via zeta potential can be used to understand and control
409 coagulation and flotation of algae, irrespective of morphological differences. Zeta
410 potential is now being used in understanding practical issues related to the coagulation
411 of NOM rich waters within a region of the UK and has resulted in lower residuals,
412 more stable systems and lower coagulant demands in certain sites (Sharp et al., 2007).
413 Surface area also provided a relationship with coagulant demand which could be
414 utilised to understand changes in dose requirements as different species predominate
415 in feed reservoirs. In contrast, monitoring cell counts without reference to species,
416 will not give an indication of coagulant demand as, on a per cell basis, the coagulant
417 demand required for optimum removal varied between species by orders of
418 magnitude. Similarly, monitoring algae with respect to taxonomic grouping will not
419 give any indication as to the coagulant demand.

420 *Insert Figure 5*

421 **Conclusions**

422 Specific conclusions are as follows:

- 423 1. Addition of coagulant to algae systems caused a neutralisation of the negative
424 charge of both cells and AOM even at pH 7, although the efficiency of
425 neutralisations varied with differing system characteristics.

- 426 2. Good cell removal efficiencies in the range 94-99 % were obtained for all
427 algae treated provided sufficient coagulant was added.
- 428 3. High MW, protein-rich AOM appears to act as a polymer aid in *M. aeruginosa*
429 systems, resulting in the absence of a restabilisation zone at pH 5.
- 430 4. AOM removal efficiency was in the range 46-71 %.
- 431 5. Residual aluminium was always low provided sufficient coagulant had been
432 added to ensure the maximum removal efficiency of AOM had been achieved.
- 433 6. A strong correlation between charge density and coagulant dose was observed
434 for all algae species at pH 7. The indications are that charge measurements
435 would provide a robust control for algae irrespective of physical and chemical
436 characteristics.

437

438 Further work is required to assess the application of such a model to real systems as
439 opposed to those artificially created using laboratory monocultures. It is anticipated
440 that the principles of the charge dependent process described in this paper should be
441 applicable in such a situation.

442

443 **Acknowledgements**

444 The authors would like to thank the EPSRC, Anglian Water, Northumbrian Water,
445 Thames Water, and Yorkshire Water for their financial support.

446 **References**

447 Bernhardt, H. and Clasen, J. (1991) Flocculation of micro-organisms. Aqua London
448 40(2), 76-87.

- 449 Bernhardt, H. and Clasen, J. (1994) Investigations into the flocculation mechanisms of
450 small algal cells. *Aqua London* 43(5), 222-232.
- 451 Bernhardt, H., Hoyer, O., Schell, H. and Lusse, B. (1985) Reaction mechanisms
452 involved in the influence of algogenic matter on flocculation. *Zeitschrift für Wasser-
453 und Abwasser-forschung* 18(1), 18-30.
- 454 Chen, C., Zhang, X.j., Zhu, L.x., Liu, J., He, W.j. and Han, H.d. (2008) Disinfection
455 by-products and their precursors in a water treatment plant in North China: Seasonal
456 changes and fraction analysis. *Science of the Total Environment* 397(1-3), 140-147.
- 457 Clasen, J., Mischke, U., Drikas, M. and Chow, C. (2000) An improved method for
458 detecting electrophoretic mobility of algae during the destabilisation process of
459 flocculation: Flocculant demand of different species and the impact of DOC. *Journal
460 of Water Supply: Research and Technology - AQUA* 49(2), 89-101.
- 461 Duan, J. and Gregory, J. (2003) Coagulation by hydrolysing metal salts. *Advances in
462 Colloid and Interface Science* 100-102(SUPPL.), 475-502.
- 463 Edzwald, J.K. (1993) Algae, bubbles, coagulants, and dissolved air flotation. *Water
464 Science and Technology* 27(10), 67-81.
- 465 Edzwald, J.K. (1995) Principles and applications of dissolved air flotation. *Water
466 Science and Technology* 31(3-4), 1-23.
- 467 Haider, S., Naithani, V., Viswanathan, P.N. and Kakkar, P. (2003) Cyanobacterial
468 toxins: A growing environmental concern. *Chemosphere* 52(1), 1-21.

- 469 Han, M., Kim, W. and Dockko, S. (2001) Collision efficiency factor of bubble and
470 particle (α_{bp}) in DAF: theory and experimental verification. *Water Science and*
471 *Technology* 43(8), 139-144.
- 472 Henderson, R., Chips, M., Cornwell, N., Hitchins, P., Holden, B., Hurley, S., Parsons,
473 S.A., Wetherill, A. and Jefferson, B. (2008a) Experiences of algae in UK waters: A
474 treatment perspective. *Water and Environment Journal* 22(3), 184-192.
- 475 Henderson, R., Parsons, S.A. and Jefferson, B. (2008b) The impact of algal properties
476 and pre-oxidation on solid-liquid separation of algae. *Water Research* 42(8-9), 1827-
477 1845.
- 478 Henderson, R., Sharp, E., Jarvis, P., Parsons, S. and Jefferson, B. (2006) Identifying
479 the linkage between particle characteristics and understanding coagulation
480 performance. *Water Science and Technology: Water Supply* 6, 31-38.
- 481 Henderson, R.K., Baker, A., Parsons, S.A. and Jefferson, B. (2008c) Characterisation
482 of algogenic organic matter extracted from cyanobacteria, green algae and diatoms.
483 *Water Research* 42(13), 3435-3445.
- 484 Henderson, R.K., Parsons, S.A. and Jefferson, B. (2008d) Successful removal of algae
485 through the control of zeta potential. *Separation Science and Technology* 43(7), 1653-
486 1666.
- 487 Jekel, M.R. and Heinzmann, B. (1989) Residual aluminium in drinking water
488 treatment. *Journal of Water Supply: Research and Technology - AQUA* 38, 281-288.
- 489 Kam, S.-K. and Gregory, J. (2001) The interaction of humic substances with cationic
490 polyelectrolytes. *Water Research* 35(15), 3557-3566.

- 491 Kempeneers, S., Menxel, F.V. and Gille, L. (2001) A decade of large scale experience
492 in dissolved air flotation. *Water Science and Technology* 43(8), 27-34.
- 493 Nguyen, M.L., Westerhoff, P., Baker, L., Hu, Q., Esparza-Soto, M. and Sommerfeld,
494 M. (2005) Characteristics and reactivity of algae-produced dissolved organic carbon.
495 *Journal of Environmental Engineering* 131(11), 1574-1582.
- 496 Petrusovski, B., Vlaski, A., Van Breeman, A.N. and Alaerts, G.J. (1993) Influence of
497 algal species and cultivation conditions on algal removal in direct filtration. *Water*
498 *Science and Technology* 27(11), 211-220.
- 499 Pieterse, A.J.H. and Cloot, A. (1997) Algal cells and coagulation, flocculation and
500 sedimentation processes. *Water Science and Technology* 36(4), 111-118.
- 501 Pivokonsky, M., Kloucek, O. and Pivokonska, L. (2006) Evaluation of the production,
502 composition and aluminum and iron complexation of algogenic organic matter. *Water*
503 *Research* 40(16), 3045-3052.
- 504 Rosen, B.H., MacLeod, B.W. and Simpson, M.R. (1992) Accumulation and release of
505 geosmin during the growth phases of *Anabaena circinalis* (Kutz.) Rabenhorst. *Water*
506 *Science and Technology* 25(2), 185-190.
- 507 Sharp, E., Borrill, B., Goslan, E. and Jefferson, B. (2007) A mechanistic approach to
508 predict disinfection by-product precursor removal during conventional coagulation,
509 *Chemical Water and Wastewater Treatment* Hahn, H.H., Hoffmann, E. and Ødegaard,
510 H. (eds), IWA Publishing, London, UK.
- 511 Sharp, E.L., Parson, S.A. and Jefferson, B. (2006) Coagulation of NOM: Linking
512 character to treatment. *Water Science and Technology* 53(7), 67-76.

513 Stumm, W. and O'Melia, C. (1968) Stoichiometry of coagulation. Journal of the
514 American Water Works Association 60, 514-539.

515 Takaara, T., Sano, D., Konno, H. and Omura, T. (2004) Affinity isolation of algal
516 organic matters able to form complex with aluminium coagulant. . Water Science and
517 Technology: Water Supply 4(5-6), 95-102.

518 Teixeira, M.R. and Rosa, M.J. (2006) Comparing dissolved air flotation and
519 conventional sedimentation to remove cyanobacterial cells of *Microcystis aeruginosa*.
520 Part I: The key operating conditions. Separation and Purification Technology 52(1),
521 84-94.

522 Tilton, R.C., Murphy, J. and Dixon, J.K. (1972) The flocculation of algae with
523 synthetic polymeric flocculants. Water Research 6(2), 155-164.

524 Widrig, D.L., Gray, K.A. and McAuliffe, K.S. (1996) Removal of algal-derived
525 organic material by preozonation and coagulation: Monitoring changes in organic
526 quality by Pyrolysis-GC-MS. Water Research 30(11), 2621-2632.

527

528

Figure and Table Headings

Figure 1. Coagulant dose:charge equivalent ratio vs. zeta potential at pH 7 for **A.** the entire system (cells and AOM) and **B.** the extracted AOM.

Figure 2. Dose response curves depicting coagulant demand in terms of surface area at pH 5 and 7 for **A.** zeta potential, and for normalised removal based on cell count for **B.** *C. vulgaris* and **C.** *M. aeruginosa*.

Figure 3. Normalised AOM removal achieved by coagulation and flotation at pH 7 using aluminium sulphate.

Figure 4. Normalised residual aluminium upon coagulation and flotation of AOM at pH 7 using aluminium sulphate, where **A.** shows all results, and **B.** shows results where residual aluminium is less than 2 %.

Figure 5. The relationship between coagulant demand for maximum removal and both charge density and surface area of the algae systems with literature data (Bernhardt and Clasen 1994, Henderson et al. 2008b).

Table 1. Key AOM characteristics for *C. vulgaris*, *M. aeruginosa*, *A. formosa* and *Melosira* sp. at pH 7 (adapted from Henderson et al. (2008c))

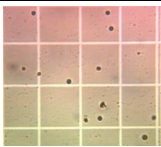

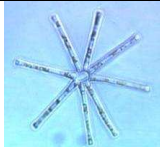



Table 2. Key cell characterisation data for *C. vulgaris*, *M. aeruginosa*, *A. formosa* and *Melosira* sp.

Table 3. Summary data for coagulation conditions required for maximum removal at pH 7.

Table 1.

	<i>Chlorella vulgaris</i>	<i>Microcystis aeruginosa</i>	<i>Asterionella formosa</i>	<i>Melosira</i> sp.
AOM (ng cell ⁻¹)	0.0029	0.00095	0.019	0.65
Charge Density (meq g ⁻¹)	3.2	0.1	1.0	Neg.
Hydrophobicity (%)	11	30	20	32
Carbohydrate:DOC (mg as glucose mg ⁻¹ as C)	1.1	0.7	1.0	0.8
Trans-/hydrophilic carbohydrates (%)	95	77	90	83
Protein:DOC (mg as Bovine Serum Albumin mg ⁻¹ as C)	0.40	0.64	0.19	0.16
Protein:carbohydrate (mg mg ⁻¹)	0.4	0.6	0.2	0.2
AOM >30 kDa (%)	62	55	9	30
AOM <1 kDa (%)	30	38	81	53

Table 2.

	<i>Chlorella vulgaris</i>		<i>Microcystis aeruginosa</i>		<i>Asterionella formosa</i>	<i>Melosira sp.</i>
	pH 5	pH 7	pH 5	pH 7	pH 7	pH 7
Cell images						
Initial Cell concentration (cells ml ⁻¹)	$5.0 \times 10^5 \pm 5 \times 10^4$	$6.0 \times 10^5 \pm 1.5 \times 10^4$	$5.0 \times 10^4 \pm 1.2 \times 10^4$	$1.9 \times 10^3 \pm 550$		
Surface area (μm ² cell ⁻¹)	55 ± 30	95 ± 34	370 ± 95	5500 ± 845		
AOM concentration (mg L ⁻¹ as C)	1.5 ± 0.15	0.6 ± 0.01	1.0 ± 0.2	1.2 ± 0.4		
Charge Equivalents per cell (including associated AOM) (peq cell ⁻¹)	0.004	0.011	negligible	0.002	0.062	1.88
% Charge Contributed by	-	84	-	5	30	negligible

AOM

ACCEPTED MANUSCRIPT

Table 3

	<i>Chlorella vulgaris</i>	<i>Microcystis aeruginosa</i>	<i>Asterionella formosa</i>	<i>Melosira sp.</i>
Optimum Coagulant Dose (in terms of cell number, surface area and charge density)				
pg cell ⁻¹	4.3	1.1	31.4	290
g m ⁻²	0.078	0.012	0.085	0.053
mg meq ⁻¹	383	927	508	154
Optimum Zeta Potential (mV)	-14.5 ± 1.6	-10 ± 2.2	-13.5 ± 0.4	1.4 ± 0.3
Optimum Cell Removal (%)	94.8	97.3	98.8	99.7

Figure 1

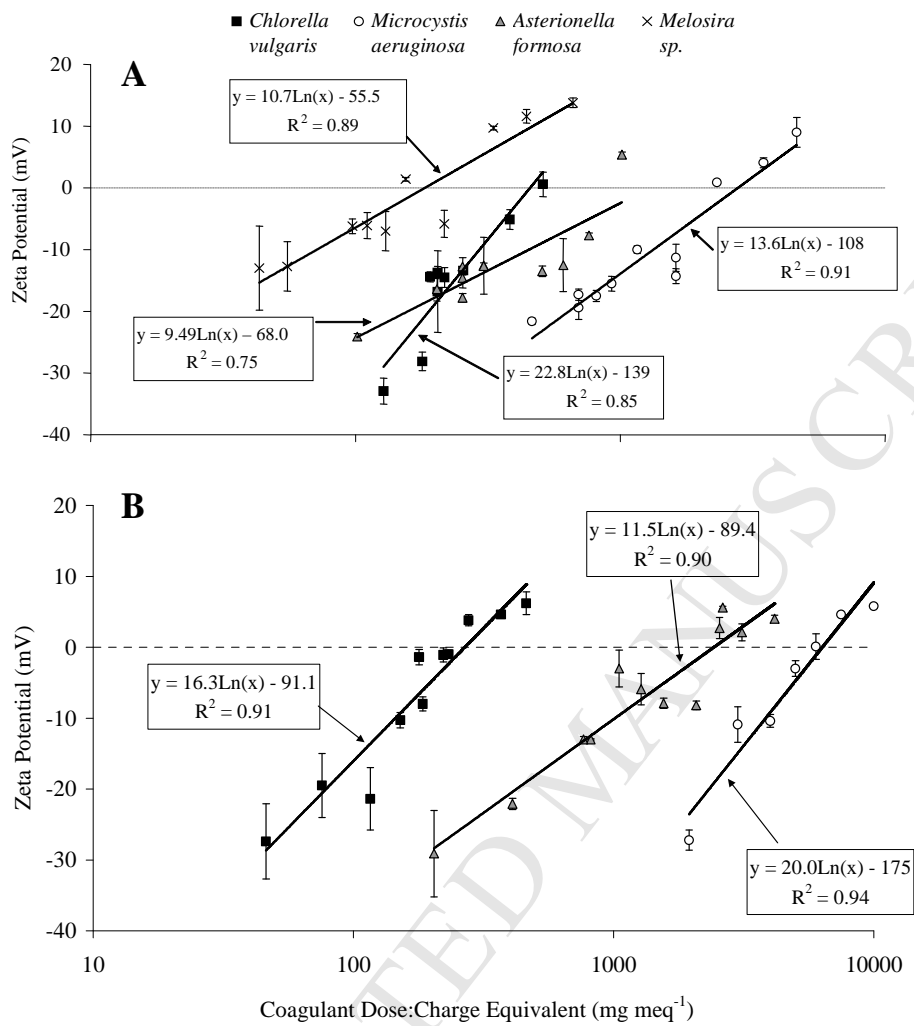


Figure 2

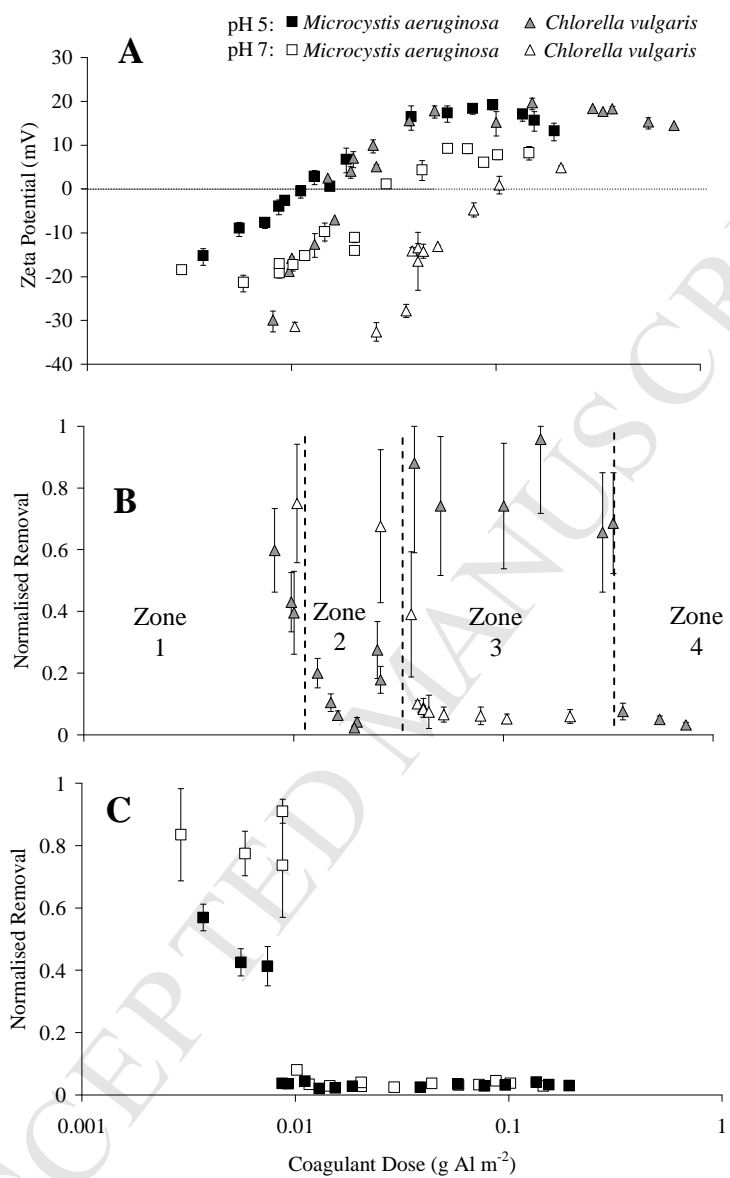


Figure 3

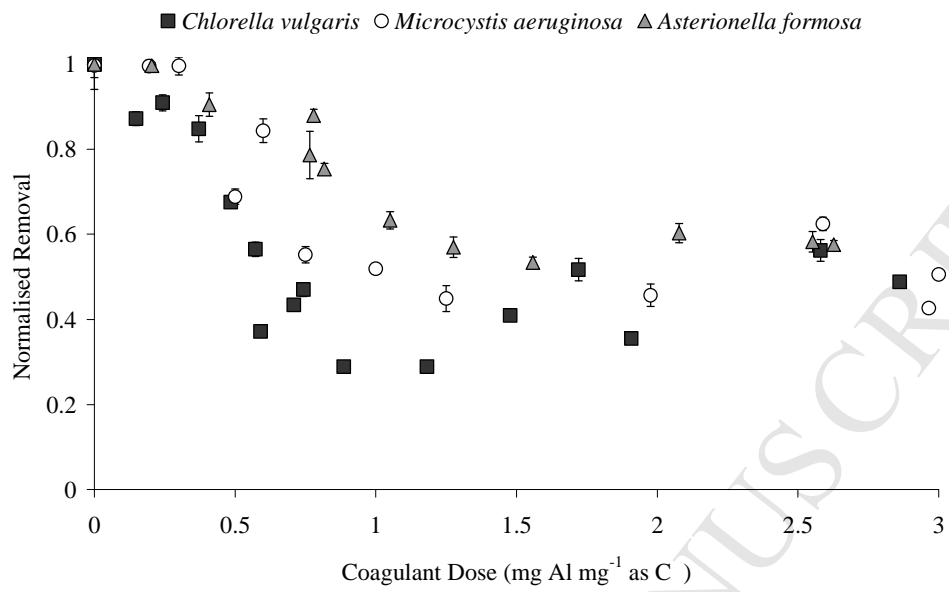


Figure 4

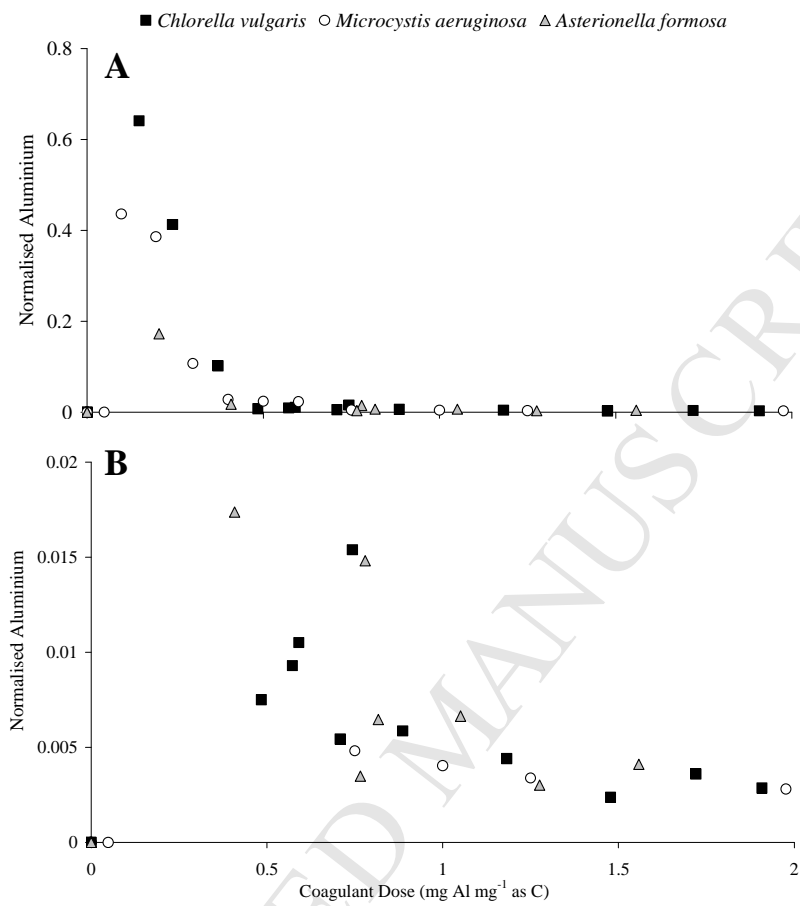


Figure 5

