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# Hydrothermal carbonization of microalgae for phosphorus recycling

# from wastewater to crop-soil systems as slow-release fertilizers

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#### 1 Abstract

2 Due to the finite stocks of phosphate rock and low phosphorus (P) use efficiency 3 (PUE) of traditional mineral P fertilizers, more sustainable alternatives are desirable. 4 One possibility is to culture microalgae in wastewater to recover the P and then 5 convert the microalgae biomass into slow-release fertilizers through hydrothermal 6 carbonization (HTC). Therefore, this study aimed to recycle P from wastewater to 7 agricultural field using microalgae and HTC technology. Chlorella vulgaris (CV) and 8 Microcystis sp. (MS) were cultured in poultry farm wastewater with an initial concentration of 41.3 mg P kg<sup>-1</sup>. MS removed 88.4% P from the wastewater, which 9 10 was superior to CV. CV- and MS-derived hydrochars were produced at 200 or 260°C, 11 in solutions using deionized water or 1wt% citric acid. The MS-derived hydrochar 12 using 1 wt% citric acid solution at 260 °C (MSHCA260) recovered the highest 13 amount of P (91.5%) after HTC. The charring promoted the transformation of soluble 14 and exchangeable P into moderately available P (Fe/Al-bound P), and using citric acid 15 solution as feedwater increased the P recovery rate and formation of Fe/Al-bound P. 16 With the abundant moderately available P pool, hydrochar amendment released P 17 more slowly and enhanced the soil P availability more persistently than chemical 18 fertilizer did, which helped to improve PUE. In a wheat-cultivation pot experiment, 19 MSHCA260 treatment improved wheat PUE by 34.4% and yield by 21.6% more than 20 chemical fertilizer did. These results provide a novel sustainable strategy for recycling 21 P from wastewater to crop-soil systems, substituting the mineral P fertilizer, and 22 improving plant PUE.

Keywords: hydrochar; microalgae technology; phosphorus fractionation; phosphorus
use efficiency; sustainable development; wheat

### 25 **1. Introduction**

26 Phosphorus (P) is an essential plant nutrient and makes up around 0.2% of plant 27 dry weight (Václavková et al., 2018; Adegbeye et al., 2020). Nevertheless, soil P 28 exists in pools of low availability and thus becomes one of the major factors limiting 29 crop growth, affecting approximately 30% agricultural fields worldwide (Xu et al., 30 2019; B. Li et al., 2020). Consequently, a vast amount of P fertilizers is required for 31 agricultural production. However, P-based synthetic fertilizers rely on P extracted 32 from phosphate rock which is a finite non-renewable resource that might be depleted 33 in 50-100 years (Withers et al., 2020). In addition, crops take up only 30-45% of the 34 supplied P from synthetic P fertilizer (Shen et al., 2011; Oita et al., 2020). The P that 35 is not incorporated into the plants is washed into waterbodies through leaching and 36 runoff, causing environmental issues (Pan et al., 2018; Lee et al., 2020). Therefore, it 37 is crucial to seek alternatives to chemical fertilizers and to develop methodologies that 38 improve P use efficiency (PUE) by crops, while minimizing the negative 39 environmental impacts.

40 Wastewater contains plentiful P that requires removal prior to discharge into 41 watercourse. Microalgae have been shown to grow rapidly in such wastewater, 42 efficiently removing P (Cabanelas et al., 2013; Subramaniyam et al., 2016; Huo et al., 43 2020). Microalgae are capable of absorbing inorganic P in excess through storage 44 within their cells in the form of polyphosphate granules (Delgadillo-Mirquez et al., 45 2016)(Solovchenko et al., 2019). Previous studies reported that microalgae can 46 accumulate large quantities of P (up to 2-4% of their cell dry weight), and thus have 47 potential to be applied as fertilizer after appropriate processing (Cabanelas et al., 2013; 48 Santos and Pires, 2018; Luo et al., 2019). Therefore, reclaiming P from wastewater 49 streams with microalgal cultures is a sustainable and environmental-friendly solution 50 to the shortage of phosphate rock. In the last decade, direct application of dried 51 microalgae as an alternative to chemical P fertilizer has been evaluated (Ray et al., 52 2013; Mukherjee et al., 2015; Schreiber et al., 2018). A major concern is that the

polyphosphate-rich biomass releases the phytoavailable P too slowly into soil to satisfy the demands of growing plants. Moreover, microalgal toxins, such as microcystin and cyanotoxin, potentially threatens both soil microbial activity and plant growth if microalgae are directly applied to soil (Machado et al., 2017). These factors have driven the researchers to explore additional treatments to enhance the fertilizer values of microalgal biomass prior to its use in an agricultural context.

59 One such potential tool for increasing PUE is the application of biochar 60 (Anyaoha et al., 2018; Bornø et al., 2018; Fei et al., 2019; H. Li et al., 2020). 61 Pyrolysis is the thermal treatment of biomass in absence of air at temperatures of 62 400-600°C, converting dry biomass into pyrochar (Foong et al., 2020). Hydrothermal 63 carbonization (HTC) converts wet biomass to hydrochars at lower temperature 64 (180-260 °C) (Hao et al., 2018; Cui et al., 2020). The higher hydrothermal 65 temperature than 260°C might lead to the increased generation of noxious compounds 66 in hydrochars, including phenols and organic acids (Hao et al., 2018). Compared with 67 pyrolysis, HTC is generally more energy-efficient and, since it is carried out in water, 68 wet microalgae can be directly processed without prior dehydration (Lachos-Perez et 69 al., 2017). More importantly, the hydrolysis reaction occurring in HTC process can 70 promote the degradation of polyphosphate into orthophosphate, with over 90% P 71 present as orthophosphate in sewage sludge- or manure-derived hydrochars 72 (Heilmann et al., 2014; Huang and Tang, 2016; Idowu et al., 2017). In addition, the 73 predominant chemical P fraction in hydrochars is iron (Fe)/ aluminum (Al)-bound P 74 (Huang and Tang, 2016; Wang et al., 2017), which is considered a moderately labile P 75 pool for plants and acting as a buffer for available P in soil (Yao et al., 2013; 76 Heilmann et al., 2014; Fei et al., 2019).

Biochar can also improve soil health by increasing soil electrical conductivity (EC), organic matter content, surface area, and nutrient availability (Bornø et al., 2018; Yu et al., 2019; Chu et al., 2020c). The microporous structures, surface functional groups, and intrinsic minerals of hydrochar could improve the capacity of nutrients adsorption and retention in soil (Yu et al., 2019; Chu et al., 2020a, 2020c), potentially avoiding P loss and improving plant PUE. Also, remarkable alterations of the

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microbial community structure in biochar-amended soil have been reported (Ye et al.,
2019; Lu et al., 2020), possibly by affecting phosphatase activity secreted by soil
microorganisms and consequently, by P solubilization. These beneficial properties,
plus the increased moderately labile P pool present within microalgae-derived
hydrochars, are likely to improve the PUE, nutrients retention, and crop growth.

This study aims to achieve P recycling from wastewater to food through the recovery of P from wastewater using microalgae, converting the biomass into hydrochar by HTC, and applying the microalgae-derived hydrochars to a crop-soil system. The specific objectives of this work included 1) investigating the fate of P from wastewater to hydrochar and then to the crop-soil system; 2) screening the most suitable microalgae-derived hydrochar to improve the PUE compared to traditional synthetic P fertilizer.

95 **2. Methods and materials** 

#### 96 2.1. Microalgal cultivation and harvest

97 Chlorella vulgaris strain CCAP 211/12 and Microcystis sp. strain CCAP 98 1450/13 were used in this study and purchased from Culture Collection of Algae and 99 Protozoa (CCAP), Scottish Marine Institute, Scotland. The wastewater was collected 100 from the poultry farm at Nottingham Trent University's Brackenhurst Campus and 101 filtered before culturing microalgae. The trials of P removal from wastewater by 102 culturing microalgae were carried out in 3 L borosilicate bioreactors in the 103 glasshouase of Brakenhurst campus, Nottingham Trent University, UK. The culturing conditions were: constant aeration (4 mL  $s^{-1}$ ), photoperiod of 14h:10h light:dark 104 cycles, at a controlled temperature of  $25 \pm 1^{\circ}$ C under cool white fluorescent light of 105 106 10000 lux intensity. The chemical characterization of wastewater is shown in Table **S1**. The initial total P (TP) concentration in the wastewater was 41.3 mg  $L^{-1}$ . Three 107 108 replicates were conducted for each microalgal strain. The dry weight (DW) of 109 microalgae was gravimetrically assessed every two days according to standard 110 method 2540-D (APHA, AWA, WPCF 1992) and reached the stationary phase in 111 wastewater after 14 days. Also, TP of wastewater was analyzed every two days using 112 an auto analyzer (AQ400, SEAL Analytical GmbH, Germany) in order to monitor the 113 P removal rate. At the end of culture total nitrogen (TN) were measured 114 colorimetrically as nitrate after the water samples had been oxidized and total organic 115 carbon (TOC) were measured using an organic carbon analyzed by an organic carbon 116 analyzer (TOC-C<sub>CSN</sub>, Shimadzu). Afterwards, the microalgae were collected by flocculation. The methods of flocculation were the same as detailed in our previous 117 118 study (Li and Pan, 2013), and are included in the Supplementary Information. The 119 flocculation efficiency of both CV and MS was more than 95% (Fig. S1).

#### 120 2.2. Microalgae-derived hydrochars preparation

121 HTC of microalgae was conducted in a 600 mL Teflon lined stainless steel hydrothermal reactor (Parr Instruments, Moline, IL, USA), using a solid:liquid ratio 122 123 of 1:9 (w/w). The wet microalgal biomass was directly mixed with the feedwater and 124 the final solid/liquid ratio was calculated based on the moisture content. Eight types 125 of hydrochars were produced using two different microalgae under two different 126 feedwaters (deionized water and 1 wt.% citric acid solution) and two different 127 reaction temperatures (200 and 260 °C). For each run, the reactor was heated to 200 or 260 °C at 3 °C min<sup>-1</sup>, and held at the final temperature for a duration of 2 h. The 128 129 pressures originating from feedwater alone at the respective reaction temperatures 130 were not monitored. The reactor was rapidly cooled down to room temperature using 131 a recirculating condensing engine. The solid and liquid products were initially 132 separated by centrifugation and fully gravity-filtered through a 0.45 µm membrane. 133 The total solid recovery rate was recorded.

#### 134 2.3. Characterization of microalgae-derived hydrochars

The pH of the hydrochars was analyzed using a solid/deionized water ratio of 136 1:2.5 (w/v). The specific surface area (SSA) and porosity were measured using a 137 NOVA 1200 analyzer (Anton Paar QuantaTec Inc., Graz, Austria), and were calculated by the Brunauer-Emmett-Teller method (Yu et al., 2019). Total C, H, N,
and S contents were determined using an Elemental Analyzer (EL III; elemental
Analysensysteme GmbH, Germany). Concentrations of metallic elements, including
K, Al, Ca, Fe, and Mg were determined by firstly digesting the hydrochars using
HNO<sub>3</sub> (61%) with hydrogen peroxide and then analyzing the digests using inductively
coupled plasma-optical emission spectrometry (ICP-OES), as described in a previous
study (Chu et al., 2019).

145 The sequential extraction of the microalgae-derived hydrochars were carried out 146 to evaluate the fractions of P present, following previous studies (Hedley et al., 1982; 147 Bornø et al., 2018) as shown in Fig S2. P fractionation in chars can be separated into 148 soluble P, exchangeable P, alkaline-dissolved and organic P, acid-dissolved and 149 organic P, and residual P fractions. The solids were separated from the extract after 150 each batch of extraction via centrifugation at 8000 g for 5 min, and the supernatant 151 was filtered using a 0.45 µm membrane filter. The P concentrations in extracts were 152 analyzed colorimetrically by auto-analyzer. TP concentrations of hydrochars were calculated by summation of all the P fractions. The P recovery rate was calculated 153 154 according to the following formula:

155 
$$P_{\text{recover}} = (P_{\text{total}} \times \lambda / P_{\text{feedstock}}) \times 100\%$$

156 where  $P_{total}$  is the TP content in the hydrochar,  $P_{feedstock}$  the TP content in the feedstock, 157 and  $\lambda$  represents the yield of the hydrochar.

158 2.4. Soil incubation experiment

159 The soil used in the incubation experiment was collected from the top soil of 160 Embleys farm in the UK (0-15 cm; 29% clay, 42% silt, 29% sand). The soil had the following basic properties: pH 7.7, organic matter content 2.1%, EC 0.52 mS cm<sup>-1</sup>, 161 cation exchange capacity (CEC) 2.42 cmol kg<sup>-1</sup>, total N 1.2 g kg<sup>-1</sup>, TP 0.63 g kg<sup>-1</sup>, 162 total K 3.2 g kg<sup>-1</sup>, Olsen-P 12.1 mg kg<sup>-1</sup>. Soils and hydrochars were air-dried, sieved 163 164 through 2 mm mesh, and mixed to ensure a relatively homogeneous distribution. 100 165 g of the top soil were placed in the 200 mL transparent plastic jars for soil incubation 166 experiments. The jars were covered with loose lids to allow air circulation but to

167 minimize water evaporation. Treatments were as follows: Untreated soil (no chemical fertilizers or hydrochars were applied), control (chemical fertilizers were applied), CV 168 169 (dried powder of *Chlorella vulgaris*), CVHCA200 (CV-derived hydrochar using 1 wt%) 170 citrate acid solution as feedwater; 200 °C HTC), MS (dried powder of Microcystis 171 sp.), MSHCA260 (MS-derived hydrochar using 1 wt% citric acid solution as 172 feedwater; 260 °C HTC). CVHCA260 and MSHCA260 were selected because they 173 had the highest P recovery rate of the Chlorella vulgaris- or Microcystis sp.-derived hydrochars. The chemical fertilization control contained 500 mg N kg soil<sup>-1</sup> in the 174 form of NH<sub>4</sub>NO<sub>3</sub>, 100 mg P kg soil<sup>-1</sup> in the form of KH<sub>2</sub>PO<sub>4</sub>, and 300 mg K kg soil<sup>-1</sup> 175 176 in the form of K<sub>2</sub>SO<sub>4</sub>. In the hydrochar treatments, the application rate of hydrochars 177 was 0.5 wt% of the soil and chemical fertilizers were additionally supplemented to 178 achieve the equivalent rates with the N, P, and K rates used in the chemical 179 fertilization control. Each treatment comprised four replicates. Incubation lasted for 180 120 days in an illuminated incubator at 25 °C. The soils were sampled at 0, 10, 30, 50, 181 80, and 120 days. During the incubation period, deionized water was added every two 182 days to maintain a field water-holding capacity at 60% (w/w).

183 2.5. Wheat pot experiment

The experiments used 5L plastic pots, each of four kilograms of air-dried soil 184 185 sieved to pass through a 2 mm mesh. A filter paper was placed at the bottom of the 186 pots to prevent soil loss. Before cultivating wheat, hydrochars were mixed with soil 187 and the pots were incubated for four weeks in a greenhouse under moderately moist 188 conditions (60% field water-holding capacity). Wheat seeds were pre-germinated in a 189 petri dish covered with a filter paper and kept in the dark for three days. After the 190 preincubation period, five germinated wheat seedlings were carefully transplanted to 191 each pot and thinned to one after one week. The design of treatments was the same as 192 described in the soil incubation experiment (2.4). Each treatment comprised four 193 replicates.

194The wheat plants were harvested at the tillering (20 days after transplantation)195and maturation stages (120 days after transplantation). In order to satisfy the

196 requirement of sampling at two different growth stages, two batches of experiments 197 were conducted at the same time. Rhizosphere soil samples were collected by 198 carefully cleansing the soil from the roots (Chu et al., 2017; Sha et al., 2020). The soil 199 samples were divided into two parts: one portion was freshly prepared for the 200 determination of enzyme activity and soil microbial C and P content, and another 201 portion was air-dried for analysis by sequential P fractionation. In fresh soil samples, 202 the concentration of microbial biomass C (MBC) and P (MBP) were investigated 203 using the chloroform fumigation-extraction method (Brookes et al., 1982). Acid and 204 alkaline phosphatase activities in the soil samples were determined as described in a 205 previous study (Bornø et al., 2018). In dried soil samples, the soil pH was analyzed in 206 a slurry of 1:2.5 (w/v, soil to water) using a pH-meter. Soil organic matter (SOM) was measured using the potassium dichromate oxidation method. Soil total N (TN) was 207 208 determined by initially digesting with H<sub>2</sub>SO<sub>4</sub> (98%) and then using the Kjeldahl 209 method (Chu et al., 2016a). CEC was measured using the compulsive exchange 210 method with 1.0 M ammonium acetate extraction at pH 7.0 (Brookes et al., 1982). 211 The analysis of soil P fractionation was same for the hydrochars, as described above 212 (2.3).

213 2.6. Statistical analyses

All statistical analyses were performed using SPSS version 23.0 (SPSS Inc. Chicago, IL, USA). One-way analysis of variance (ANOVA) was used to evaluate the significant difference at a P < 0.05 probability level with Duncan's multiple range test.

218 **3. Results** 

#### 219 3.1. Growth of microalgae and P removal in the wastewater

The microbial growth curves were plotted showing the values of biomass (as dry weight) in wastewater versus time (in days) (**Fig 1**). CV and MS both exhibited exponential growth and reached a stationary phase after 8 days. After 14 days culture,

the biomass (dry matter) of MS reached the maximum value (1.14  $g_{dw} L^{-1}$ ), 8.5% 223 224 higher than that of CV (Table S2). The average biomass productivities of CV and MS were 0.068 and 0.071  $g_{dw} L^{-1} d^{-1}$ , respectively. The plot of P removal in the 225 wastewater versus time (in days) is also shown in Fig 1. From 0 to 8 days, the P 226 concentration in the MS culture declined from 41.3 to 4.8 mg  $L^{-1}$ , with a daily P 227 removal rate of 2.95 mg  $L^{-1}$  day<sup>-1</sup>, and in the CV culture from 41.3 to 8.8 mg  $L^{-1}$ , 228 with a daily P removal rate of 2.32 mg  $L^{-1}$  day<sup>-1</sup>(**Table S2**). After 14 days culture, the 229 maximum P removal rate by MS was 10.7 mg  $L^{-1}$  day<sup>-1</sup>, which was 23.4% higher 230 231 than that of CV (Table S2). Overall, after 14 days culture, MS and CV removed 88.4% and 78.7% P, respectively, from an initial concentration of 41.3 mg P  $L^{-1}$ ; both 232 233 microalgae were demonstrated to be able to remove and enrich P from wastewater 234 efficiently although MS was superior to CV in this respect. In addition to the P 235 removal, after 14 days the TN concentration in CV and MS culture declined from 321.6 mg  $L^{-1}$  to 182.1 and 160.4 mg  $L^{-1}$ , TOC from 375.2 to 53.2 and 34.8 mg  $L^{-1}$ , 236 237 respectively, suggesting that with the fast growth the microalgae possibly absorbed and assimilated the N and C at a high rate from the wastewater as well. 238

#### 239

#### 3.2. Basic physiochemical characteristics of hydrochars

The physiochemical characteristics of the microalgae and microalgae-derived 240 241 hydrochars are displayed in Table 1. The microalgae-derived hydrochars using 242 deionized water as feedwater all exhibited an alkaline pH after processing. Using 243 citric acid as feedwater markedly neutralized the alkalinity of hydrochars from 7.2-8.5 244 to 5.7-6.6. With hydrothermal temperature decreasing from 260 °C to 200 °C, the 245 lower pH was observed in hydrochars, irrespective of microalgae strain. Transforming 246 the microalgae into hydrochars decreased the C, H, N, and S concentration, 247 irrespective of microalgae strain (Table 1). As a consequence of the vaporization, 248 degradation, and dissolution processes of labile fractions occurring during HTC, 249 elements including C, H, N, and S were partially lost to feedwater, whereas 250 conservative elements such as P and metals were retained in the hydrochars (Table 1 251 and 2). The C concentration in hydrochars using citric acid as feedwater ranged from 53.9-66.2%, which is 1.5-6.3% higher than that in hydrochars where deionized water
was used as feedwater, while H and N concentration decreased, resulting in higher
C/N and lower H/C ratio.

255 Moreover, the hydrochars using citric acid as feedwater showed a markedly 256 higher concentration of metals, including Al, Ca, Fe, and Mg, irrespective of 257 microalgal strain processed (Table 1). The increased abundances of these elements 258 were possibly beneficial for P bonding in hydrochars. Additionally, as a metal with 259 high mobility, K in hydrochars showed an opposite trend to other metals. Using citric 260 acid as feedwater during HTC reduced K accumulation in hydrochars compared to 261 those when using deionized water. In addition, different reaction conditions during 262 HTC changed the adsorptive capacity of hydrochars (Table 1). When compared to the 263 raw microalgae, hydrochars markedly increased the SSA and porosity. The SSA for hydrochars using citric acid as feedwater during HTC ranged from 5.8-6.7 m<sup>2</sup> g<sup>-1</sup>, 264 265 which was 16.6-18.2% higher than that in hydrochars using only deionized water as 266 feedwater.

#### 267 3.3. Recovery rate of P in hydrochars

268 As displayed in Table 2, the charring process resulted in an increased P content 269 in the hydrochars. The P content in CV-derived hydrochars ranged from 3.4±0.2-270 4.3±0.4 %, which was 23.1-67.9% higher than that of raw CV, and in MS-derived 271 hydrochars ranged from  $4.2\pm0.3-5.8\pm0.4\%$ , which was 14.7-72.2% higher than that of 272 raw MS. Moreover, with increasing hydrothermal temperature from 200 to 260°C the 273 TP increased from 3.2-4.1% to 3.5-4.1% in CV-derived hydrochars, and from 3.9-5.4% 274 to 4.5-6.2% in MS-derived hydrochars. In addition, TP in MS-derived hydrochars 275 varied from 3.9-6.2%, which was 21.9-31.9% higher than that in CV-derived 276 hydrochars. This result might be attributed to the higher P uptake by MS in 277 wastewater (Fig. 1).

With hydrothermal temperature increasing from 200 °C to 260 °C, in contrast with P recovery, the solid recovery rate of hydrochars declined from 40.7-49.8% to 37.3-45.4% in CV-derived hydrochars, and from 44.6-58.8% to 42.1-55.2% in

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281 MS-derived hydrochars. This result might be ascribed to the degradation of polymeric 282 materials (such as hemicellulose and cellulose) at higher temperatures during HTC. 283 Moreover, using citric acid solution as feedwater during HTC markedly increased the 284 hydrochar yield and TP, irrespective of microalgal strain. The solid recovery rate of 285 microalgae-derived hydrochars using citric acid solution ranged from 41.1-62.0%, but 286 that of hydrochars using deionized water ranged from 32.3-46.3%. Also, for CV, P 287 content in CVHCA200 and CVHCA260 was 9.4-27.0% higher than that in 288 CVHW200 and CVHW260; for MS, P concentration in MSHCA200 and MSHCA260 289 was 21.6-28.2% higher than that in MSHW200 and MSHW260. The highest P 290 recovery rate for CV and MS were both attained by using citric acid as feedwater, 291 72.3% in CVHCA260 and 91.5% in MSHCA260.

#### 292 3.4. Fractionation of P in hydrochars

293 The results of the sequential P fractionation of the microalgae and 294 microalgae-derived hydrochars are presented in Fig. 2. The charring process 295 significantly reduced soluble, exchangeable, and residual P fractions, but increased 296 largely the Fe/Al-bound and Ca-bound P fractions. The soluble and exchangeable P 297 generally correspond to the phytoavailable P. This phytoavailable P constituted 34.0% 298 of the Chlorella vulgaris and 27.9% of the Microcystis sp., whereas less than 20% 299 was detected in derived hydrochars (e.g., 8.8% in MSHCA260) (Table S5). 300 Additionally, with increasing hydrothermal temperature from 200 to 260 °C, the 301 soluble P fraction decreased sharply, irrespective of microalgal strains.

302 However, the charring process significantly improved the Fe/Al-bound P 303 fraction by 2.1-3.4 and 1.7-3.8 fold for CV and MS, and the Ca-bound P fraction by 304 2.7-4.7 and 1.4-2.5 -fold for CV and MS, respectively (Fig. 2). Fe/Al-bound P was the 305 largest P fraction in microalgae-derived hydrochars, ranging from 32.8-52.7%. In 306 addition, using citric acid solution as feedwater during HTC significantly increased 307 the Fe/Al- and Ca-bound P fractions. The Fe/Al- and Ca-bound P in CVHCA200, 308 CVHCA260, MSHCA200, and MSHCA260 ranged from 15.2-30.5% and 5.8-12.6%, 309 which was 23.6-64.0% and 7.4-90.9% higher than those in CVHW200, CVHW260,

310 MSHW200, and MSHW260, respectively. Using citric acid solution as feedwater 311 probably better facilitated the bonding between those metallic elements present and P.

Overall, HTC promoted the P transformation from readily available and recalcitrant fractions to potentially available fractions and using citric acid as feedwater sharpened such transformation. Fe/Al-bound P occupied 46.2% and 51.5% in CVHCA260 and MSHCA260, but only 19.5% and 20.1% in the raw CV and MS (**Table S5**), suggesting that P release in hydrochars will be possibly more sustainable for satisfying the long-term demand of plant growth.

#### 318 *3.5.P release from microalgae-derived hydrochars to soil*

319 The raw microalgae and microalgae-derived hydrochars were incubated in the 320 soil for 120 days, in order to investigate the release capacity of phytoavailable P, as 321 shown in Fig. 3. The unfertilized soil and soil applied with chemical fertilizers were 322 regarded as control groups. CVHCA260 and MSHCA260 were selected in this 323 experiment because of their highest TP (Table 2) and highest moderately labile P pool 324 (Fig. 2) among the respective microalgae-derived hydrochars. At 10 days after 325 incubation, the available P concentration in soils treated with chemical fertilizer was 326 remarkably and consistently higher than that in other treatments. However, after 50 327 days, the two hydrochar treatments, CVHCA260 and MSHCA260, significantly and 328 persistently improved the concentration of soil available P compared to the chemical 329 fertilizer group. At 120 days after incubation, the soil available P concentration under 330 CVHCA260 and MSHCA260 treatment was 47.7% and 56.3% higher than that for 331 the chemical fertilizer group, respectively. In addition, from 10 to 30 days the 332 available P concentration in soils treated with CV and MS were consistently higher 333 than those treated with CVHCA260 and MSHCA260, however, an opposite trend was 334 observed from 30 to 120 days after incubation. At 120 days after incubation, soil 335 available P concentration under CVHCA260 treatment was 10.9% higher than that 336 under CV treatment, and under MS260 treatment was 21.0% higher than that under 337 MS treatment. From 50 to 120 days, the highest soil available P concentration was consistently detected in the MSHCA260 treatment, although a decreasing trend wasdetected for all the groups.

#### 340 3.6. Rhizosphere soil properties

341 properties of rhizosphere soils amended with microalgae The or 342 microalgae-derived hydrochars at the ripening stage of wheat are shown in Table S6. 343 CVHCA260 and MSHCA260 significantly reduced soil pH by 0.4-1.6 units compared 344 to the control. CV, MS, CVHCA260, and MSHCA260 significantly improved the 345 SOM by 19.8%, 12.3%, 25.8%, and 26.6% respectively compared to that in control. 346 Also, amendment by MSHCA260 significantly improved the CEC compared to the 347 control and the two microalgae-derived hydrochars significantly improved the CEC 348 compared to the control, and to the CV- and MS- amended soils. Moreover, with 349 addition of CV and MS, soil total N was maintained at a similar level to that of the 350 control, however, amendment by CVHCA260 and MSHCA260 significantly reduced 351 soil TN by 33.3% and 42.9%, respectively, compared to the control. Because of 352 effects on SOM and TN, CV and MS addition significantly increased soil C/N ratio 353 compared to control, by 62.3% and 92.4% for CVHCA260 and MSHCA260 354 respectively.

355 The incorporation of microalgae and microalgae-derived hydrochars to soil 356 affected microbial activity, as shown in the results of soil phosphatase activity in Fig. 357 S3 and MBC and MBP content in Fig. S4. The introduction of C from microalgae or 358 microalgae-derived hydrochars into soil significantly improved the soil MBC, 359 irrespective of the growth stages, compared to the control. However, soil MBP 360 displayed different results. At the tillering stage, no significant difference was 361 detected for MBP, while at the ripening stage, CV and MS addition significantly 362 reduced MBP by 26.2% and 33.9% compared to the control, and significantly lower 363 MBP were detected in CVHCA260 and MSHCA260 treatment (reduced 71.9% and 364 79.5%). Different treatments affected the phosphatase activity in rhizosphere soil. No 365 significant differences were detected for acidic phosphatase activity among treatments. 366 However, alkaline phosphatase activity significantly improved either at tillering or

ripening stages for CV, MS, CVHCA260, and MSHCA260 treatments when
compared to the control; alkaline phosphate activity in the rhizosphere soil under
CVHCA260 and MSHCA260 treatments was 39.5-42.9% higher than that under CV
and MS treatment at the tillering stage, and 51.7-56.0% higher at the ripening stage.

#### 371 3.7. *P* fractionation in rhizosphere soil of wheat

372 The results of the sequential P fractionation of rhizosphere soil from a wheat pot 373 experiment are shown in Fig. 4. The results of labile and stable P pools in the 374 rhizosphere soil are shown in Fig. S5. Notably, the addition of CV, MS, CVHCA260, 375 and MSHCA260 significantly reduced soluble P by 4.9-, 3.8-, 3.5-, and 3.6-fold, and 376 exchangeable P by 47.4%, 82.6%, 80.5%, and 68.3%, respectively, at the tillering 377 stage. However, an opposite varying trend was observed at the ripening stage; the 378 addition of CV, MS, CVHCA260, and MSHCA260 increased soil labile P pool (sum 379 of soluble and exchangeable P fraction) by 1.7-, 1.6-, 1.8-, and 2.1-fold compared to 380 the control, respectively (Fig. S5). Compared to CV and MS, MSHCA260 treatment 381 resulted in a higher labile P pool at the ripening stage, suggesting that addition of 382 CVHCA260 could maintain a higher level of soil available P for a longer period.

383 Fe/Al-bound P is defined as the moderate P pool because the P bound to Fe and 384 Al (hydr)oxides is not directly absorbed by plants but gradually becomes soluble. The 385 significantly higher Fe/Al-bound P concentrations were detected at the tillering stage 386 in the soils treated with CV, MS, CVHCA260, and MSHCA260, whereas the opposite 387 trend was detected at the ripening stage (Fig. 4C). In contrast with these treatments, 388 the Fe/Al-bound P in the control became higher as plants matured, suggesting that, at 389 an early growth stage of wheat, the readily available P from chemical P fertilizer 390 became gradually bound to Fe and Al (hydr)oxides. Despite the highest Fe/Al-bound 391 P concentration (Fig. 2) among all hydrochars, the lowest soil Fe/Al-bound P fraction 392 was detected in the MSHCA260 treatment at the ripening stage (Fig. 4C).

The sums of Ca-bound P and residual P fractions were defined as the stable P pool, because Ca-bound P usually corresponds to apatite and residual P corresponds to recalcitrant P-containing clay mineral (Hedley et al., 1982). Unlike the labile and 396 moderately available P pool, soil Ca-bound and residual P pool kept relatively stable 397 after the addition of CV, MS, CVHCA260, or MSHCA260 (Fig. 4D and 4E). No 398 significant difference was detected for soil Ca-bound P or residual P fraction among 399 treatments except at the ripening stage, where addition of MSHCA260 significantly 400 reduced the soil Ca-bound P fraction compared to the control.

401 *3.8. PUE and yield of wheat* 

402 The results of PUE and yields of wheat grain are shown in Fig. 5. CV, 403 CVHCA260, and MSHCA260 treatment significantly improved the plant PUE by 404 32.4%, 35.3%, and 34.4% compared to the control (Fig. 5A). Compared to the raw 405 CV, amendment by microalgae-derived hydrochars did not significantly improved the 406 PUE. However, among four treatments only MSHCA260 significantly improved the 407 wheat grain yield by 21.6% (Fig. 5B). In addition, despite statistically insignificant 408 difference, CVHCA260 treatment improved the grain yield by 14.5% compared to the 409 control.

## 410 **4. Discussions**

#### 411 *4.1. Recovery of P from wastewater and conversion to microalgae-derived hydrochars*

412 With the development of "Enhanced biological P removal", microalgae-based 413 techniques are attracting increased attention because of the luxury uptake of P by 414 microalgae, accumulating P up to 2-4% of their cell dry weight (Cabanelas et al., 415 2013; Santos and Pires, 2018; Luo et al., 2019). The cost of wastewater treatment 416 must be counterbalanced with efficacy of P removal and production of microalgal 417 biomass, which further produces a significant economic benefit to society (Prasad et 418 al., 2014; Solovchenko et al., 2019). In this study, after 14 days culture in the poultry wastewater with an initial concentration of 41.3 mg P  $L^{-1}$ , MS and CV removed 88.4% 419 420 and 78.7% P, respectively, showing a strong capacity to remove P from wastewater. 421 Table S4 compared the P removal efficiencies obtained in this study with the results 422 in previous studies. This comparison showed that with the increased initial P

423 concentration in influent wastewater the P removal efficiency became higher. In the 424 present study, MS and CV removed the P from wastewater (with initial P concentration of 41.3 mg  $L^{-1}$ ) at 2.95 and 2.32 mg  $L^{-1}$  day<sup>-1</sup>; in previous studies 8.39 425 mg  $L^{-1}$  day<sup>-1</sup> P removal rate was observed from the wastewater at initial P 426 concentration of 128.2 mg  $L^{-1}$  (Luo et al., 2019) and 0.55 mg  $L^{-1}$  day<sup>-1</sup> P removal rate 427 from the wastewater at initial P concentration of 8.0 mg  $L^{-1}$  (Tao et al., 2017). These 428 429 results were likely attributed to the stimulated biosynthesis and storage of 430 polyphosphate to cope with the external stress of excessive P concentration (Mujtaba 431 et al., 2017; Shen et al., 2017; Powell et al., 2009; Solovchenko et al., 2016, 2019).

432 Polyphosphate is the dominant P speciation in microalgae (Powell et al., 2009; 433 Solovchenko et al., 2019) and generally recalcitrant to degradation, making it largely 434 unavailable for plants. HTC has been demonstrated to be able to promote degradation 435 by polyphosphate hydrolysis in feedwater. Hence, in the present study the enriched P 436 in microalgae was transferred to hydrochars by HTC. The P concentrations in 437 microalgae-derived hydrochars ranged from 3.2-6.2% (Table 2), which were notably higher than hydrochars derived from animal manure and crop residuals (<3%) 438 439 (Heilmann et al., 2014; Wang et al., 2017; Fei et al., 2019). This result demonstrated 440 that luxury P uptake by microalgae from wastewater played an important role in producing the P-rich hydrochars. In addition, with increasing hydrothermal 441 442 temperature from 200 to 260°C, the hydrochar yields were observed to decrease but 443 the P recovery rate increased, irrespective of feedwater or microalgal strain (Table 2). 444 A similar trend has been reported in the HTC treatment of swine manure (Heilmann et 445 al., 2014), wetland plants (Cui et al., 2020), and sewage sludge (Huang and Tang, 446 2016). The cracking of biopolymers and P precipitation during HTC might be 447 responsible for the higher P accumulation in higher temperature-derived hydrochars 448 (Dai et al., 2015; Ekpo et al., 2016). The composition of feedwater was demonstrated 449 to be an important factor for hydrochar yield and P recovery rate. Using 1% citric acid 450 solution as feedwater significantly improved these parameters, irrespective of reaction 451 temperature or microalgae strain. Using citric acid solution as feedwater likely 452 promoted the bonding between metal cations and phosphate. Use of acidic feedwater

has previously been demonstrated to promote the release of metal cations in
hydrochars (Idowu et al., 2017; Yuan et al., 2018; Cui et al., 2020) and in the
transformation of organic P to inorganic P (Heilmann et al., 2014; Wang et al., 2017).

456 Differing reaction temperatures and feedwater composition in the HTC process 457 affected the P fractionation in the resulting hydrochars (Fig. 2). The charring of 458 microalgae significantly reduced the soluble, exchangeable, and residual P fractions, 459 but increased the Fe/Al-bound and Ca-bound P fractions. Similar results have been 460 reported where 44.3% readily available P was detected in the raw sewage sludge but 461 only 7.5% was detected in the derived hydrochars (Fei et al., 2019). During HTC 462 some orthophosphate dissolved into the feedwater and was lost, whereas most other P 463 species bonded and adsorbed with various metals to increase retention on the 464 hydrochars (Zhang et al., 2016). A larger proportion of microalgal P was chemisorbed 465 by Fe/Al (hydr)oxides compared to that by Ca-containing compounds, which is 466 comparable with hydrochars derived from sewage sludge (Huang and Tang, 2016; Fei 467 et al., 2019), but extremely different from animal manure and other plant biomass 468 where Ca-bound P is dominant (Heilmann et al., 2014; Dai et al., 2015; Bornø et al., 469 2018; Cui et al., 2020). Because PAC was used as a reagent to flocculate and collect 470 the microalgae after culturing in wastewater (Fig S1), a larger amount of AlCl<sub>3</sub> was 471 possibly remained in the microalgae and promoted the formation of the Al-bound P 472 fractions, as reflected in the Al concentration of hydrochars (0.9-2.8%). Notably, 473 using 1% citric acid solution as feedwater significantly increased the Fe/Al-bound P 474 fraction in these hydrochars, irrespective of microalgal strains or reaction temperature, 475 achieving 46.2% and 51.5% in CVHCA260 and MSHCA260. Importantly, these 476 Fe/Al-bound P fractions can be desorbed in soil and slowly released as phytoavailable 477 species (Yao et al., 2013; Heilmann et al., 2014; Fei et al., 2019), avoiding the P 478 leaching or runoff due to overly fast dissolution, which occurs with chemical P 479 fertilizer (Koppelaar and Weikard, 2013; Sha et al., 2018; Liu et al., 2020). The 480 Fe/Al-bound P fractions are considered as moderately available and act as a buffer for 481 available P in soils (Wang et al., 2014; Zhang et al., 2016; Cui et al., 2020). The loss 482 of a readily-available P pool during the HTC was more than made up for by a much

larger increase in Fe/Al-bound P that eventually can be slowly released into the soil tosupport plant growth.

# 485 4.2. Application of microalgae-derived hydrochars to a crop-soil system as 486 slow-release P fertilizer

487 Soil incubation and wheat pot experiments both revealed that the 488 microalgae-derived hydrochars supplied the soil with a pool of slowly-releasable P, 489 and consequently, the plants with more sustainable P nutrition than did traditional 490 chemical P fertilizer. In the soil incubation experiment, amendment with CVHCA260 491 and MSHCA260 persistently improved the soil available P from 50 to 120 days (Fig 492 3). In the wheat pot experiment, CVHCA260 and MSHCA260 amendment 493 significantly improved the soil soluble and exchangeable P fractions (Fig. 4A and 4B). 494 The abundant Fe/Al-bound P pool in hydrochars could be an important reason for the 495 observed slow-release of P. Sewage sludge-derived hydrochars have been 496 demonstrated to transform the available P fraction from raw sludge to an Fe/Al-bound 497 P fraction after HTC, possessing a strong capacity to release P in electrolyte solution 498 (Huang and Tang, 2016; Fei et al., 2019). Similar results were also reported in the persistent increase in the soil labile P pool, following amendment with crop 499 500 residue-derived biochars (Xu et al., 2016; Bornø et al., 2018). These results suggest 501 that chemical P fertilizer was beneficial for increasing soil P availability at an early 502 stage of plant growth whereas microalgae and microalgae-derived hydrochars were 503 able to supply P to plants over a longer term. However, prior to utilization by plants 504 the initial pulse of fast-release P from a chemical P fertilizer could possibly be lost by 505 leaching, runoff, and assimilation by soil organisms, as reflected by the significantly 506 higher soil MBP in the control (Fig. S4).

507 As the wheat grew, it is possible that the pool of moderately available P treated 508 with microalgae-derived hydrochars gradually transformed to the labile P pool. This 509 effect is similar with the application of organic and slow-release fertilizer (Chu et al., 510 2016b; Václavková et al., 2018). Root activity, leading to the exuding of organic acids 511 into soil, and phosphatase excreted by soil microorganisms might have driven such 512 transformation (Shen et al., 2018). In the present study, the amendment of 513 CVHCA260 and MSHCA260 greatly improved the alkaline phosphatase activity in 514 the rhizosphere both at tillering and ripening stages (Fig. S3). HTC promoted the 515 hydrolysis of macromolecules from microalgae cells, such as polyphosphate and 516 proteins, to produce a large amount of low weight molecules in the resulting 517 hydrochars (Bornø et al., 2018; Yu et al., 2019; Chu et al., 2020b). It is speculated that 518 these low weight molecules were readily assimilated by soil microorganisms and thus 519 increased microbial activity or, possibly caused a shift in the composition of the 520 microbial community, resulting in increased levels of alkaline phosphatase, 521 concomitantly increasing soil available P. Moreover, the charring process significantly 522 improved the SSA and porosity (Table 1). Higher SSA and increased porous volume 523 levels are extremely important for improving nutrient retention in soil because they 524 can facilitate higher mass transfer fluxes and adsorption loading of soil nutrients 525 (Bornø et al., 2018; Chu et al., 2020a; Lu et al., 2020), which might be another reason 526 for the maintaining higher soil available P over a long term.

527 With the persistently improved soil available P pool in the rhizosphere, 528 microalgae-derived hydrochar treatments significantly improved plant PUE (Fig. 5A). 529 Notably, however, compared to CV, CVHCA260 and MSHCA260 were observed not to significantly improve plant PUE. A possible reason might be that improved P 530 531 availability due to hydrochar addition exceeded the demand of plant growth. In the 532 soil incubation experiment, the labile P pool of soils treated with hydrochars were still 533 far higher than those of most arable soils (< 20 mg kg<sup>-1</sup>) and even in excess of the recommended P application rate (40-50 mg kg<sup>-1</sup>) in agricultural fields (Sha et al., 534 535 2018; Václavková et al., 2018; H. Li et al., 2020). Therefore, in future studies, a 536 reduced application rate of hydrochars will be attempted. In addition, despite all four 537 treatments increasing PUE, only MSHCA260 significantly increased the yield of 538 wheat grain (Fig. 5B), perhaps because as well as improved soil P availability, 539 increases soil C/N, SOM, CEC could also be contributing (Table S6). These factors 540 are beneficial for nutrient mineralization and retention in soil and root morphology 541 (Shen et al., 2011; Xu et al., 2014; Lu et al., 2020), which might also help promote

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542 wheat yield production. In addition, a slightly alkaline soil (pH 7.7) was used in the 543 present study and the CHVCA260 and MSHCA260 addition lowered the soil pH to 544 6.4 and 6.6, respectively (Table S6). The lowering soil pH was beneficial for 545 dissolving Ca-bound P and facilitating hydrochars to provide more adsorption sites 546 between Fe/Al and P compounds. In the present study only deionized water and 1% 547 citric acid were used as feedwater. In case the feedwater with higher pH is attempted 548 to produce hydrochars, e.g., 2-5% citric acids, would be acidic and thus possibly aggravate the soil acidification. Although lowering soil pH might be helpful for the 549 550 increase of Fe/Al-bound P pool, the soil acidification is also harmful for root 551 respiration and growth, as shown in the previous study that poplar sawdust-hydrochar 552 with pH of 3.7 inhibited rice growth and yield greatly (Yu et al., 2019). Further 553 studies should carry on to investigate the effects of different feedwater pH on P 554 recovery in hydrochars.

In recent years the synergistic effects of hydrochar application together with chemical fertilizer on crop yield have been widely reported (Bornø et al., 2018; Yu et al., 2019; Chu et al., 2020a, 2020c). However, importantly, this study for the first time demonstrated a substitutive role of hydrochars over chemical P fertilizer to improve crop production.

#### 560 **5. Conclusions**

561 The microalgae, CV and MS, both showed a strong ability for the removal of P 562 from P-rich wastewater, and MS was superior to CV in this respect. After 14 days culture in wastewater, MS removed 88.4% P from wastewater at 2.65 mg  $L^{-1}$  dav<sup>-1</sup>. 563 564 Then 91.5% P were recovered from the raw MS to the hydrochar MSHCA260. The 565 P-enriched microalgae-derived hydrochars behaved as a slow-release P fertilizer to 566 satisfy the long-term demand of growing wheat. MSHCA260 amendment improved 567 the plant PUE by 34.4% and yield production by 21.6%. The findings from this study 568 can be used to develop sustainable and eco-friendly strategies to recycle P from 569 wastewater to agricultural fields for food production, which has the positive dual 570 effects of saving the cost of wastewater treatment and the production of a valuable 571 slow-release P fertilizer to alleviate the possible future shortage of phosphate rock. A 572 limitation of the present study is that the microalgal culture was conducted using a 573 batch experiment under a fixed initial P concentration. The large-scale outdoor 574 experiments where the influent flow of wastewater keeps feeding are worthy of 575 carrying out to simulate the industrial wastewater process and quantify the P removal 576 efficiency by microalgae. Also, the microalgae-derived hydrochars did not improve 577 significantly the PUE compared to the raw microalgae. Thus, follow-up works are 578 required to carry out before the large-scale field trials. Further modifications such as 579 loading metal cations to ameliorate the P chemisorption can be attempted in addition 580 to using citric acid solution as HTC feedwater.

#### 581 **Conflicts of interests**

582 The authors declare no competing financial interest

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#### 590 Author contributions

591 QC designed the experiments; GP and LX acquired the funding and supervised the 592 research; QC, TL, BY, and MC performed the experiments; QC analyzed the data; YF 593 and LY visualized the work; QC wrote the manuscript; TL, RM, LY, and MC 594 reviewed and edited the manuscript; QC, GP, and LX finalized the manuscript.

#### 595 Supplementary Information

596 Detailed information about the materials and methods for microalgae flocculation, 597 chemical properties of wastewater, the maximum biomass concentration, maximum 598 biomass productivity, average biomass productivity, maximum P removal rate, and 599 average P removal rate determined for CV and MS, the concentration of TN, TP, and 600 TOC in the effluent of wastewater after culturing CV and MS, comparisons between P 601 removal efficiencies and average P removal rated obtained in this study and previous studies reporting microalgal in different wastewater effluents, mass content and 602 603 relative abundance of different P fractions in raw microalgae and microalgae-derived 604 hydrochars, the properties of rhizosphere soils amended with microalgae or microalgae-derived hydrochars at ripening stage of wheat, flocculation efficiency and 605 606 zeta potential for flocculating microalgae, overview of the sequential P fractionation 607 procedure performed on hydrochar and soil samples, acid and alkaline phosphatase activity in the rhizosphere soil, microbial biomass C and P in the rhizosphere soil, 608 609 labile and stable P pool in the rhizosphere soil, are presented in the **Supplementary** 610 Information.

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#### **Captions to illustrations**

 Table 1. Basic physiochemical characteristics of raw microalgae and microalgae-derived hydrochars.

**Table 2**. Hydrochar yield, total P content and P recovery of the microalgae-derived hydrochars (n=3).

**Figure 1**. Growth curves of *Chlorella vulgaris* and *Microcystis sp.* and dynamic variation of P concentration in poultry farm wastewater.

Figure 2. Fractionation of P in sequential extracts of raw microalgae and microalgae-derived hydrochars.

**Figure 3.** The dynamic variation of soil available P with the application of chemical fertilizer, raw microalgae and microalgae-derived hydrochars during 120 days incubation.

**Figure 4**. P fractionation in the rhizosphere soil grown with wheat, including (A) soluble P fraction, (B) exchangeable P fraction, (C) Fe/Al-bound P fraction, (D) Ca-bound P fraction, and (E) residual P fraction.

**Figure 5**. Wheat PUE (A) and grain yield (B) in a pot experiment. Each value was the average of results from four replicates.

Table 1. Basic physiochemical characteristics of raw microalgae and microalgae-derived hydrochars. Values are means  $\pm$  SE of three independent measurements.

	CV	CVHW200	CVHW260	CVHCA200	CVHCA260	MS	MSHW200	MSHW260	MSHCA200	MSHCA260
рН <sup>а</sup>	$8.2 \pm 0.3$	$7.4 \pm 0.2$	$7.6 \pm 0.4$	$6.1 \pm 0.1$	$6.5 \pm 0.1$	$8.0 \pm 0.5$	$7.9 \pm 0.3$	$8.3 \pm 0.2$	$5.9 \pm 0.2$	$6.4 \pm 0.1$
$C(\%)^{b}$	$63.8 \pm 2.9$	$55.6 \pm 3.5$	$56.4 \pm 1.8$	$60.5 \pm 5.7$	$59.3 \pm 2.4$	$65.6 \pm 1.8$	$58.7 \pm 3.6$	$57.2 \pm 3.2$	$60.3 \pm 6.4$	$61.0 \pm 3.7$
H (%)	$4.1 \pm 0.2$	$4.1 \pm 0.4$	$4.4 \pm 0.2$	$3.3 \pm 0.1$	$3.8 \pm 0.3$	$4.0 \pm 0.1$	$3.8 \pm 0.1$	$3.4 \pm 0.1$	$3.0 \pm 0.1$	$3.2 \pm 0.2$
N (%)	$10.8\pm0.4$	$8.7 \pm 0.7$	$7.3 \pm 0.6$	$8.1 \pm 0.4$	$6.2 \pm 0.5$	$12.3 \pm 0.7$	$10.2 \pm 0.4$	$9.2 \pm 0.6$	$9.5 \pm 1.1$	$8.8 \pm 0.7$
S (%)	$2.7 \pm 0.2$	$1.5 \pm 0.1$	$0.4 \pm 0.03$	$1.4 \pm 0.1$	$0.8 \pm 0.09$	$2.2 \pm 0.2$	$1.3 \pm 0.03$	$0.6 \pm 0.04$	$1.5 \pm 0.1$	$0.6 \pm 0.03$
K (%)	$1.8 \pm 0.1$	$1.5 \pm 0.2$	$1.1 \pm 0.1$	$1.3 \pm 0.07$	$0.9\pm0.05$	$1.6 \pm 0.2$	$1.2 \pm 0.1$	$1.3 \pm 0.06$	$1.1 \pm 0.2$	$0.8 \pm 0.04$
Al (%)	$0.8\pm0.05$	$1.1 \pm 0.2$	$1.2 \pm 0.2$	$1.8 \pm 0.3$	$1.9 \pm 0.3$	$1.0 \pm 0.1$	$1.7 \pm 0.2$	$1.7 \pm 0.1$	$2.2 \pm 0.3$	$2.4 \pm 0.4$
Ca (%)	$1.1 \pm 0.07$	$1.3 \pm 0.2$	$1.5 \pm 0.1$	$2.2 \pm 0.3$	$2.4 \pm 0.2$	$0.9 \pm 0.08$	$1.2 \pm 0.1$	$1.3 \pm 0.2$	$1.8 \pm 0.08$	$2.1 \pm 0.3$
Fe (%)	$0.7\pm0.04$	$0.9 \pm 0.1$	$1.1 \pm 0.06$	$1.5 \pm 0.1$	$1.6 \pm 0.2$	$0.4 \pm 0.03$	$0.8\pm0.05$	$0.8 \pm 0.08$	$1.3 \pm 0.1$	$1.5 \pm 0.06$
Mg (%)	$0.1\pm0.02$	$0.3 \pm 0.04$	$0.4\pm0.02$	$0.6 \pm 0.05$	$0.6 \pm 0.04$	$0.08\pm0.01$	$0.1\pm0.007$	$0.2 \pm 0.04$	$0.4 \pm 0.03$	$0.05\pm0.06$
$SSA (m^2 g^{-1})^c$	$0.6\pm0.02$	$5.4\pm0.05$	$5.7\pm0.02$	$6.6 \pm 0.07$	$6.4 \pm 0.06$	$0.4 \pm 0.04$	$5.2 \pm 0.04$	$5.0\pm0.06$	$5.9 \pm 0.06$	$6.1 \pm 0.05$
Porosity	$0.004 \pm$	$0.05 \pm$	$0.03 \pm$	0.06 ±	$0.04 \pm$	$0.002 \pm$	$0.03 \pm$	$0.02 \pm$	$0.04 \pm$	$0.03 \pm$
$(cm^3 g^{-1})$	0.0005	0.006	0.003	0.008	0.005	0.0003	0.004	0.003	0.006	0.004

a. The pH was determined by a pH meter using a solid/Milli-Q water ratio of 1:2.5 (w/v).

b. The total elemental concentrations of C, H, N, and S were determined by an Elemental Analyzer (EL III; Elementar Analysensysteme GmbH, Germany). The total concentrations of elemental Al, Ca, Fe, and Mg were measured using ICP-OES.

c. SSA and porosity were measured were measured using a NOVA 1200 analyzer (Anton Paar QuantaTec Inc., Graz, Austria), and the parameters were calculated using the Brunauer–Emmett–Teller method.

Feedstock	HTC reaction medium	Sample label	Solid recovery rate (%)	Total P concentration (wt%)	P recovery (%)
Chlorella vulgaris	Raw	CV	N/A	$2.7 \pm 0.1$	N/A
	Deionized water, 200 °C	CVHW200	$40.7 \pm 3.9$	$3.4 \pm 0.2$	51.3
	Deionized water, 260 °C	CVHW260	$37.3 \pm 5.0$	$3.6 \pm 0.1$	49.7
	1 wt.% citric acid, 200 °C	CVHCA200	$49.8 \pm 3.7$	$3.8 \pm 0.3$	70.1
	1 wt.% citric acid, 260 °C	CVHCA260	$45.4 \pm 4.3$	$4.3 \pm 0.4$	72.3
Microcystis sp.	Raw	MS	N/A	$3.5 \pm 0.1$	N/A
	Deionized water, 200 °C	MSHW200	44.6 ± 1.7	$4.2 \pm 0.3$	53.5
	Deionized water, 260 °C	MSHW260	42.1 ± 5.4	$4.8 \pm 0.3$	57.4
	1 wt.% citric acid, 200 °C	MSHCA200	$58.8 \pm 3.2$	$5.2 \pm 0.2$	87.4
	1 wt.% citric acid, 260 °C	MSHCA260	$55.2 \pm 2.8$	$5.8 \pm 0.4$	91.5

**Table 2**. Hydrochar yield, total P content and P recovery of the microalgae-derived hydrochars (n=3). (N/A: not applicable)

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Figure 1. Growth curves of *Chlorella vulgaris* and *Microcystis sp.* and dynamic variation of P concentration in poultry farm wastewater. Green circles and diamonds represent the biomass and blue markers represent the P concentration in the wastewater. Values are means  $\pm$  SE of three independent measurements. The biomass was based on the dry weight (DW) of microalgae.





**Figure 2.** Fractionation of P in sequential extracts of raw microalgae and microalgae-derived hydrochars. Each data was the average of results from three independent extraction experiments. Error bars indicate SE. Means not sharing the same letter (a-e) are significantly different at the p = 0.05 level by one-way ANOVA. The abbreviations of materials are the same as those in Table 2. The relative abundance (percentage) of each P fractionation is shown in Table S2.



**Figure 3.** The dynamic variation of soil available P with the application of chemical fertilizer, raw microalgae and microalgae-derived hydrochars during 120 days incubation. Each data was the average of results from four replicates. Error bars indicate SE (n = 4). Significant differences between treatments are indicated with different letters. The abbreviations of materials are the same as those in Table 2. Soil+NPK means the soil applied with chemical N, P, and K fertilizers.





**Figure 4.** P fractionation in the rhizosphere soil grown with wheat, including (A) soluble P fraction, (B) exchangeable P fraction, (C) Fe/Al-bound P fraction, (D) Ca-bound P fraction, and (E) residual P fraction. Each data was the average of results from four replicates. Error bars indicate SE (n = 4). Columns denoted by different lowercase letters indicate statistically significant differences affected by different microalgae and microalgae-derived hydrochar treatments, and those labelled with different uppercase letters indicate significant differences for the same treatment between tillering and ripening stages. The abbreviations of materials are the same as those in **Table 2**. The sequential extraction method and explanation of different P fractions are detailed in **Fig S2**. The results of labile P pool and stable P pool are shown in **Fig S5**.



Figure 5. Wheat PUE (A) and grain yield (B) in a pot experiment. Each value was the average of results from four replicates. Error bars indicate SE (n = 4). Statistically significant differences between treatments are indicated with different letters. The abbreviations of materials are those detailed in **Table 2**.

# Highlights

- Chlorella vulgaris and Microcystis sp. (MS) removed 78.7% and 88.4% phosphorous (P)
- 91.5% P was recovered from MS to MS-derived hydrochar produced at 260 °C • (MSHCA260)
- Microalgal hydrochars slowly released P and improved soil P availability •
- MSHCA260 increased P use efficiency and wheat yield compared to chemical • fertilizer
- Microalgae and hydrochar technology recycled P from wastewater to crop food •

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# **Credit author statement**

QC designed the experiments; GP and LX acquired the funding and supervised the research; QC, TL, BY, and MC performed the experiments; QC analyzed the data; YF and LY visualized the work; QC wrote the manuscript; TL, RM, LY, and MC reviewed and edited the manuscript; QC, GP, and LX finalized the manuscript.

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#### **Declaration of interests**

 $\boxtimes$  The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests: